

THE DEVELOPMENT OF A TREATMENT SCHEME FOR A COMPLEX BASE METAL ORE FROM PRAIRIE CREEK, NORTHWEST TERRITORIES

W. ARTHUR WALL AND R. W. BRUCE

by

MINERAL PROCESSING DIVISION

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Mines Branch Investigation Report IR 70-52

THE RECOVERY OF SILVER, COPPER, LEAD AND ZINC FROM SAMPLES OF ORE SUBMITTED BY CADILLAC EXPLORATION LIMITED, (N.P.L.) PRAIRIE CREEK, NORTHWEST TERRITORIES

by

W. Arthur Wall* and R. W. Bruce**

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SUMMARY OF RESULTS

The sulphide ore sample was successfully concentrated by standard flotation methods as illustrated by the results of Test 43 which follow:

		Assay	s			Distri		
Product	Ag oz/ton	Cu %	Pb %/	Zn %	Ag	Cu	Рb	Zn
Cu conc	220.46	27.90	8.30	12.20	44.8	55.8	1.1	0.8
Pb conc	19.83	-	67.00	9.36	38.8		82.4	6.0
Zn conc	2.80	-	4.01	58.19	12.5	-	11.2	86.3
Cl tail	3.34	-	5.60	20.60	2.9	-	3.0	5.9
Ro tail	0.385	- (1)	1.35	1.08	1.0	-	2.3	1.0
Feed (calcd)	9.83	1.00 ⁽¹⁾	15.62	29.60	100.0	-	100.0	100.0

(1) Assay.

The carbonate ores represented by Samples No. 1 and 2, can be floated and satisfactory lead concentrates produced. The zinc can be floated but the production of a satisfactory grade of zinc concentrate was

*Research Scientist, and ** Head, Non-Ferrous Minerals Scetion, Mineral Processing Division, Mines Branch, Department of Energy, Mines and Resources, Ottawa, Canada.

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not achieved. If the rougher lead concentrate and rougher zinc concentrate are combined, a low grade silver, lead and zinc concentrate is obtained with satisfactory recoveries. The following table shows the assays and recoveries of the cleaned lead concentrate, the cleaned zinc concentrate and the calculated bulk concentrate of two tests.

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	Test 17 ⁽¹⁾			Test 48 ⁽²⁾			
	Weight %	Assay	Dist.%	Weight%	Assay	Dist%	
Lead conc Ag oz/ton Pb % Zn %	25.4	19.31 68.61 1.02	74.1 79.3 15.0	38.6	- 50.72 11.41		
Zinc conc Ag oz/ton Pb % Zn %	5.5	7.56 18.77 10.77	6.3 4.7 34.4	30.3	2.31 32.25		
Ro bulk conc (calcd) Ag oz/ton Pb % Zn %	57.2	11.08 37.66 2.53	95.7 98.0 83.9	74.1	28.92 20.62	3 1	

(1) Composite Sample No. 1, Lead and Zinc Concentrates cleaned once.

(2) Composite Sample No. 2, Lead and Zinc Concentrates not cleaned.

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INTRODUCTION

Location of Property

The property of Cadillac Explorations Limited (N.P.L.) is located on Prairie Creek in the Northwest Territories, one hundred and ten miles due west of Fort Simpson. The property consists of approximately 10,000 acres.

Shipments

A shipment of thirty bags of ore, each weighing approximately one hundred pounds, was received January 20, 1969. These samples had been crushed to approximately one half inch and were representative of the carbonate ore in the deposit.

On November 4, 1969, a sample of sulphide ore weighing 215 pounds was received.

Purpose of Investigation

Cadillac Exploration Limited requested an investigation to determine the amenability of the carbonate ore to flotation concentration. Upon receipt of the sulphide sample, the company requested a preliminary investigation be carried out on this sample. An intensive investigation was not warranted because this sulphide sample came from one development heading.

Sampling and Analysis

The thirty carbonate samples were composited according to instructions received from the mining company as outlined below:

Our Sample No. Components
1. Samples No. 14047, 14049, 14052, 14053, and 14057 all from No. 3 Vein, No. 3 Zone.
2. Samples No. 14032, 14033, and 14034 all from Zone 8, Trench E, footage 0'-17'.
3. Samples No. 14048, and 14050, from No. 2 Vein, No. 3 Zone, No. 3 X-cut.
4. Samples No. 14043 to 14046 all from Zone 7, Trench 1-4.

s (Cont'd)

- 5. Samples No. 14029 to 14031 from Zone 8, Trench D, footage 0'-20'.
- 6. Samples No. 14036 to 14038 from Zone 8, Trench F, footage 0'-13'.
- 7. Samples No. 14039 to 14042, from Zone 8, Trench G, H, I and J.

8. Samples No. 14026 to 14028 from Zone 8, Trenches A, B, C, and D.

Each of the composite samples Nos. 1 to 8 was crushed and sampled by conventional methods. Representative portions of Sample No. 1 were split out for microscopic examination, chemical analysis, and semiquantitative spectrographic analysis. The representative portions of the seven other composite samples were submitted for chemical analysis. Each of the thirty samples received from Cadillac Exploration Ltd. had been sampled and assayed. Using their assay results, the assays of the eight composite samples were calculated. These calculated assays have been tabulated in Table 1, beside the actual assays for comparative purposes.

TABLE 1

Sample No.	1		2		3		4	
	Head		Head		Head		Head	
Metal	Assay	Calc.	Assay	Calc.	Assay	Calc.	Assay	Calc.
Silver oz/ton	6.07	7.25	14.19	13.63	2.36	2.67	13.11	11.64
Lead % (total)	20.00	24.25	21.91	22.75	6.00	6.93	14.75	14.41
N.S. Lead % **	5.00	- ·	19.97	-	3.07	_	10.55	-
Zinc % (total)	1.72	1.79	18.35	18.87	2.96	3.24	4.45	4.56
N.S. Zinc %	1.52	-	18.26	-	2.85	-	4.34	-
Copper %	0.19	0.24	0.77	0.68	0.07	0.07	1.16	0.78
							_	
Sample No.		5	6		7		8	
	Hea	ad	Head		Head		Head	
Metal	Assay	Calc.	Assay	Calc.	Assay	Calc.	Assay	Calc.
Silver oz/ton	5.93	5.63	9.44	9.79	11.65	10.30	6.10	5.84
Lead % (total)	14.75	15.84	23.14	24.59	17.76	16.59	20.00	18.34
N.S. Lead % **	9.28	-	10.99	-	13.48	-	13.22	-
Zinc % (total)	23.00	13.99	11.50	9.41	14.00	13.02	15.00	13.48
N.S. Zinc %	22.84	-	11.38	-	13.88		14.87	-
Copper %	0.22	0.15	0.22	0.25	0.78	0.56	0.25	0.19

Chemical Analyses* of Composite Samples

* From Internal Reports MS-AC-69-448, 453, 486, 488, and 494. ** N.S. means non-sulphide

The semi-quantitative spectrographic analysis of Composite Sample No. 1 is shown in Table 2.

TABLE 2

Semi-quantitative Spectrographic Analysis* of Sample No. 1

Principal Constituent (>	1%) Si
Prominent Constituent(<	1% > 0.1%) Mg, Pb, Fe, Zn, Ni,
Minor Constituent (<	0.1%) Mn, Cr, Al, Cu, Ag, Ti
Not Detected	Sb, As, Mo, W, Sn, Bi, V, Ca, In, Zr, Co, Sr

* From Internal Report MS-AC-69-38.

The sulphide ore sample was crushed to minus one half inch. One quarter of the sample was split out and crushed to minus 10 mesh. The minus 10 mesh material was split into 1000 gram samples for chemical analysis, microscopic analysis, semi-quantitative spectrographic analysis and flotation investigative tests. The chemical analysis is reported in Table 3 and spectrographic analysis in Table 4.

TABLE 3

Chemical Analysis* of Sulphide Ore Sample

Silver	9.95 oz/ton
Lead (Total)	17.40%
N.S. Lead **	1.94%
Zinc (Total)	30.80%
N.S. Zinc	1.14%
Copper	1.00%

* From Internal Reports MS-AC-69-779 and 784 ** N.S. means non-sulphide

TABLE 4

Semi-Quantitative Spectrographic Analysis* of Sulphide Ore Sample

Major Constituent (>1%) Pb, Zn, SiProminent Constituent (<1.0% > 0.1%) Mg, Fe, Al, Ca, Cu, NiMinor Constituent (<0.1%) Cr, Mn, Ag, Ti</td>Not DetectedBa, B, Sb, Ge, As, Mo, W, Sn, Nb, Ta, In, Bi, V,Sr, Li, Zr, Na, Co

* From Internal Report MS-AC-69-670

MINERALOGICAL EXAMINATIONS

Mineralogical examinations were carried out on the carbonate ore Sample No. 1 and on the sulphide ore sample.

Carbonate Ore, Sample No. 1

A copy of the report* covering the mineralogical examination of the carbonate ore Sample No. 1 is attached as Appendix A.

The copper, lead and zinc occur both as sulphides and as carbonates and the silver in the sample occurs as a constituent of argentiferous tetrahedrite. The minerals are galena, bournonite, cerussite, sphalerite, smithsonite, covellite, enargite, chalcopyrite and malachite. Also present are pyrite, goethite, quartz, dolomite, and pyroxene.

The major lead-bearing mineral is galena with small amounts of cerussite and bournonite. Galena occurs mainly as free grains, even in the 48 to 65-mesh fraction, but to a minor degree as inclusions (5 to 70 microns in size) in sphalerite, cerussite and gangue. The cerussite is present as free grains and in association with galena and other carbonates.

Sphalerite and smithsonite are present in small quantities. The chief occurrence of sphalerite is as free grains and in association with the galena, although some occurs as inclusions in gangue and in combination with covellite. Electron-probe microanalysis of the sphalerite shows that it has a low iron content (about one percent or less).

Smithsonite occurs as free grains and in association with the other carbonates.

Argentiferrous tetrahedrite, containing about 1.3 per cent silver, occurs as free grains, as inclusions in galena and in association with bournonite and enargite.

Small amounts of copper minerals were present mainly covellite which occurs as inclusions in gangue and in association with galena and sphalerite. Minute amounts of enargite and traces of chalcopyrite and malachite were seen.

The gangue is composed essentially of quartz. Also present are a small quantity of dolomite and traces of pyroxene.

* Mines Branch Internal Report MS-69-40 by D. R. Owens.

Sulphide Ore

The microscopic examination* of the sulphide sample shows that the ore is composed essentially of massive sulphides and of small masses and grains of sulphide minerals in a largely siliceous gangue. The zinc is present in the ore as sphalerite, with the lead occurring principally as galena and as minute amounts of cerussite. Tetrahedrite accounts for nearly all of the copper although traces of the secondary copper sulphide, covellite, are also present. The presence of silver was confirmed only as trace amounts in the tetrahedrite.

Quartz greatly predominates over the other gangue minerals. Small amounts of both siderite and dolomite occur in the quartz and in the ore minerals as veinlets and inclusions.

The sphalerite, galena and tetrahedrite appear to be of a sufficiently coarse size to permit a high degree of liberation by standard milling methods although some galena may be retained in both the sphalerite and tetrahedrite as very small inclusions.

OUTLINE OF INVESTIGATION

Sample No. 1 was composited from samples of No. 3 Vein underground and was considered the most representative of the oxidized material. Consequently this sample was investigated first. Grinding and flotation testing resulted in the production of a silver-lead concentrate of satisfactory grade and with satisfactory recovery of the silver and lead. A satisfactory zinc concentrate was not produced. However, if the rougher lead and zinc concentrates are combined, as in Test 17, a bulk concentrate would be obtained. The bulk concentrate assayed 11.1 oz silver per ton, 37.7% lead and 2.50% zinc representing 95.7% of the silver, 98.0% of the lead, and 83.9% of the zinc in the feed.

The investigation was continued on Sample No. 2 which assayed 21. 91% lead and 18.35% zinc as compared with Sample No. 1 assaying 20.0% lead and 1.72% zinc. A limited amount of flotation testing was carried out with some success in the production of a zinc concentrate. This phase of the investigation was stopped when the company requested an investigation of a sample of sulphide ore from the property.

Full details of all tests are shown in the Test Data Reports in Appendix B.

* Mines Branch Investigation Report IR-70-10 by D. R. Owens.

DISCUSSION OF RESULTS

Results obtained on Composite Sample No. 1

Composite Sample No. 1 assayed 6.07 oz silver per ton, 20.0 per cent total lead, 5.0 per cent non-sulphide lead, 1.72 per cent total zinc, 1.52 per cent non-sulphide zinc and 0.19 per cent copper.

Tests 2 to 20, with the exception of Tests 3 and 7, were carried out on Composite Sample No. 1 to determine the grind, flotation conditions and reagents necessary for the production of lead and zinc concentrates. Satisfactory lead concentrates were produced (see Tests 15 and 17) but the production of satisfactory zinc concentrates was not achieved.

Tests 14 and 16 were gravity concentration tests carried out on a Wilfley Table. In each test, a satisfactory lead concentrate was produced but the zinc was concentrated into a low-grade middling product. The metal recoveries in the concentrate and middling were too low to warrant further investigation.

Test 2 was a preliminary flotation test carried out on ore ground to 66.8 per cent minus 200 mesh with the flotation conditions and reagents as shown in Table 5. The results of this test are tabulated in Table 6.

TABLE	5
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Operation	pH	Reagents	lb/ton
Grind	6.0	Aerofloat 31 Sodium Cyanide Zinc Sulphate	0.04 0.20 0.40
Condition Lead Flotation	7.0	Z-ll CaO Cresylic Acid	0.10 1.00 0.03
Zinc Condition Zinc Float	8.3	CaO CuSO ₄ Z-11 Cresylic Acid	1.00 0.50 0.10 0.03
Lead Clean Zinc Clean		n an an grund an	

Test 2 Flotation Conditions and Reagents

TABLE 6

Results	\mathbf{of}	Flotation Test 2	
	_		

Product	Wt.	Assay %				Distribution %			
	%	Ag*	Pb	Zn	Cu	Ag	Рb	Zn	Cu
Clean Pb conc	16.0	21.68	81.52	0.26	0.23	53.1	62.6	2.6	18.5
Clean Pb tail	5.2	20.73	48.39	2.48	0.84	16.5	12.1	7.8	22.0
Ro Pb conc	21.2	21.45	73.39	0.81	0.38	69.6	74.7	10.4	40.5
Clean Zn conc	2.7	12.54	24.00	3.11	0.80	5.2	3.6	5.1	11.0
Clean Zn tail	4.0	7.96	18.63	3.27	0.45	.4.9	3.6	7.9	9.0
Ro Zn conc	6.7	9.80	22.28	3.21	0.60	10.1	7.2	13.0	20.0
Bulk conc	27.9	18.65	61.12	1.38	0.43	79.7	81.9	23.4	60.5
Rougher tail	72.1	1.83	5.25	1.89	0.11	20.3	18.1	76.6	39.5
Feed (calcd)	100.0	6.53	20.80	1.65	0.20	100.0	100.0	100.0	100.0

* oz/ton

As can be seen from the above table, the separation of the lead from the zinc was not satisfactory nor was the overall recovery.

Test 4 was carried out on ore ground to 53.7 per cent minus 200 mesh with exactly the same flotation conditions and reagents as used in Test 2. The results obtained in Test 4 were similar to those of Test 2 indicating that finer grinding was not warranted.

Test 6 was carried out on ore ground to 44.0 per cent minus 200 mesh with the same reagents used in the two previous tests. The results of this test were not as good as Test 2 and 4. Test 9 was carried out on ore ground to 44.0 per cent minus 200 mesh using sodium carbonate instead of lime for alkalinity control. No zinc depressants (sodium cyanide and zinc sulphate) were used. The results of this test were not satisfactory.

Test 5 was a repeat of Test 4 with a few small changes in flotation conditions and reagents. The lime was added to the rod mill instead of during conditioning. Aerofloat 31 was used instead of cresylic acid. The pH during flotation was 6.9. The silver, lead and zinc recoveries in the lead concentrate were all higher than in Test 4. The zinc concentrate was equal in grade and recovery to the zinc concentrate in Test 4. The reagents used in Test 5 produced better results than those used in Tests 2 and 4.

Test 8 was carried out on ore ground to 53.7 per cent minus 200 mesh instead of 44.0 per cent minus 200 mesh as in Test 9. The reagents and conditions in Tests 8 and 9 were the same but somewhat different to those of Test 4. The finer grind of Test 8 resulted in an improvement of the results compared to those of Test 9 but they were still inferior to Test 4.

Tests 10, 11, 12, and 13 were carried out on ore ground to 53.7 per cent minus 200 mesh with slight changes in reagents which did not materially effect the grades of concentrates or recoveries. The concentrates were all lower in grades and recoveries than those obtained in Tests 2 and 4.

In Test 17, carried out on ore ground 53.7 per cent minus 200 mesh, Reagent 404 was used in the lead flotation and markedly increased the lead recovery. Sodium sulphide and Reagent 3037 were used in the zinc flotation and increased the zinc recovery. The rougher tailing assayed 0.67 oz silver per ton, 1.00 per cent lead and 0.65 per cent zinc and contained 4.3 per cent of the silver, 2.0 per cent of the lead and 16.1 per cent of the zinc in the feed.

Test 18 in which ammonium phosphate was used in the lead float did not produce results comparable to Test 17.

Tests 15, 19 and 20 were carried out on ore ground to 66.8 per cent minus 200 mesh with reagents very similar to those used in Test 18. The results of Test 20 were better than Test 18 but not as good as Test 17.

From the results of these tests, it is apparent that Test 17 illustrates the grind, floation conditions and reagents for the most satisfactory treatment of the ore represented by Composite Sample No. 1.

Results Obtained on Composite Sample No. 2.

Composite Sample No. 2 assayed 14.19 oz silver per ton, 21.91 per cent total lead, 19.97 per cent non-sulphide lead, 18.35 per cent total zinc, 18.25 per cent non-sulphide zinc and 0.77 per cent copper.

Tests 21, 22, 25, and 26 were conducted with similar flotation conditions and reagents but each test was conducted on ore ground to a different degree of fineness. Test 22 at a grind of 53.7 per cent minus 200 mesh produced the best results. The rougher lead concentrate assayed 42.10 per cent lead and 13.24 per cent zinc and contained 89.1 per cent of the lead and 33.3 per cent of the zinc in the feed. The rougher zinc concentrate assayed 6.21 per cent lead and 35.89 per cent zinc and contained 7.9 per cent of the lead and 54.3 per cent of the zinc in the feed.

Another series of tests (Nos. 23, 24, 45, and 46) was carried out on the ore at a grind of 53.7 per cent minus 200 mesh and with reagents similar to those used in Test 22. Each test has some slight difference in the reagents. Test 22, with the results as outlined previously, produced better results than any test in this series.

Another series of tests (Nos. 47, 48, 52 and 53) was carried out at the same grind (53.7 per cent minus 200 mesh) but with lead flotation reagents different from those used in the previous series of tests. The zinc flotation reagents were quite similar to those used in the previous tests. The concentrates produced in Test 48 are considered to be the best of those produced from this sample. In Test 48, three lead concentrates and one zinc concentrate were produced. These concentrates can be combined as shown in Table 7.

TABLE 7

Product	Weight	A	ssay %	Distribution %	
	%	Pb	Zn	Pb	Zn
No. 1 Pb conc	11.0	46.56	10.73	23.5	6.3
No. 2 Pb conc	27.6	52.37	11.69	66.4	17.2
Combined No. 1 & No. 2	38.6	50.72	11.41	89.9	23.5
No. 3 Pb conc	5.2	22.22	21.15	5.3	5.9
Zinc conc	30.3	2.31	32.25	3.2	52.3
No. 3 Pb + Zn conc	35.5	5,22	30.63	8.5	58.2
Total conc	74.1	28.92	20.62	98.4	81.7

Test 48 Flotation Concentrates

The results illustrated above are very similar to those obtained in Test 17 on Composite Sample No. 1, especially the lead grades and recoveries. In each test, the grind was 53.7 per cent minus 200 mesh and the flotation reagents used were similar.

Results Obtained on Sulphide Ore

The sulphide ore assayed 9.95 oz silver per ton, 17.40 per cent lead, 30.80 per cent zinc and 1.00 per cent copper. Tests 27 to 44 excluding Test 36 were carried out to determine the flotation conditions and reagents necessary for the production of satisfactory lead and zinc concentrates.

Three preliminary flotation tests (Nos. 27, 28, and 29) were carried out on ore ground to 74.5 per cent minus 200 mesh and each was floated with different reagent combinations. From the results of these tests, it can be seen that it was possible to float the silver, lead, zinc and copper with high recoveries. The separation of the lead and zinc into separate concentrates was not achieved in these tests.

Tests 30 and 32 were carried out on ore samples ground to 58.0 per cent minus 200 mesh and with the same flotation conditions and reagents as used in Test 29 which was carried out on ore ground to 74.5 per cent minus 200 mesh. The finer grind used in Test 29 resulted in slightly higher metal recoveries than in Tests 30 and 32.

Tests 31, 34, and 35 were carried out on ore ground to 58.0 per cent minus 200 mesh with reagents and conditions similar to those used in Test 28. Test 34 resulted in the best overall recovery but Test 35 resulted in the better lead concentrate and zinc concentrate grades and recoveries. Test 34 was also better than Test 28 or Test 29. A grind of 58.0 per cent minus 200 mesh appears to be sufficient to produce satisfactory results.

Tests 33 and 37 were carried out on ore at a grind of 91.5 per cent minus 200 mesh and with the reagents and conditions similar to those used in Test 29. Lead and zinc concentrates with satisfactory grades and recoveries were produced. The lead and zinc separation was better than that achieved in Tests 29, 30 and 32 but there was a slight decrease in recoveries.

In Test 38, sodium sulphite was used as a zinc depressant as well as sodium cyanide and zinc sulphate but it gave no improvement in zinc depression.

Test 39 was a repeat of Test 38 at a coarser grind of 74.5 per cent minus 200 mesh and with the lead float at a pH of 8.0. The results of this test were superior to Test 33, 37, and 38 which were carried out at a grind of 91.5 per cent minus 200 mesh but the results of Tests 34 and 35 at grinds of 58.0 per cent minus 200 mesh were slightly better than Test 39.

Test 40 was carried out on ore at a grind of 75.5% with sulphidization of the lead carbonate minerals with sodium sulphide. The lead-zinc separation was very good but the metallurgical recoveries were not as satisfactory as Tests 34 and 35.

Tests 41 and 42 were carried out to determine the effect of flotation at different per cent solids. In Test 41, flotation roughing was carried out at 15 per cent solids and in Test 42 at 33 per cent solids. Test 41 resulted in better lead and zinc recoveries but Test 42 at 33 per cent solids showed greater lead-zinc selectivity.

Test 43 was carried out to illustrate the results to be obtained when making a copper-lead separation. The ore was ground to 74.5 per cent minus 200 mesh and the lead-zinc flotation reagents were similar to those used in Test 29. The results are shown in condensed form in Table 8.

TABLE 8

Product	Wt.		As	say			Distril	oution	%
	% -	Ag	Cu	Pb	Zn	Ag	Cu	Pb	Zn
		oz/ton	70	%	%		(1)		
Cu conc	2.0	220.46	27.90	8.30	12.20	44.8	55.8	1.1	0.8
Pb $conc(2)$	19.2	19.83	-	67.00	9.36	38.8	-	82.4	6.0
Zn conc (3)	43.9	2.80	-	4.01	58.19	12.5	-	11.2	86.3
Zn clean tail	8.4	3.34	-	5.60	20.60	2.9	-	3.0	5.9
Rougher tail	26.5	0.38	-	1.35	1.08	1.0	-	2.3	1.0

Test 43 Flotation Results

(1) Based on 1.00% copper head assay.

(2) Combined lead concentrate and copper-lead re-recleaner tail.

(3) Combined clean zinc concentrate and copper-lead clean and reclean tail.

CONCLUSIONS

The investigation on the oxidized samples was done on Composite Sample No. 1 (No. 3 Vein, No. 3 Zone), containing 5.0 per cent non-sulphide lead and 1.5 per cent non-sulphide zinc and Composite Sample No. 2 (Zone 8, Trench E, Footage 0'-17'), containing 20 per cent non-sulphide lead and 18.3 per cent non-sulphide zinc. The remaining six samples of oxidized ore had similar assays to Sample No. 1 or Sample No. 2 and it was not considered necessary to test these as results were expected to be similar.

The results of the investigation on this ore, showed that at a relatively coarse grind of 58 per cent minus 200 mesh a satisfactory silver-lead concentrate could be floated, but no success was achieved in making a separate high-grade zinc concentrate. However, a low-grade bulk silver-leadzinc concentrate could be produced with good metal recoveries.

Selective flotation of a silver-lead concentrate gave products assaying from 50 to 68 per cent lead with 80 to 90 per cent lead recovery and 75 per cent recovery of the silver. The high recoveries were associated with the higher grade samples, (see Test 17 and 48 in appendices). In the flotation of a bulk silver-lead-zinc concentrate, containing in the order of 50 per cent of the weight of the feed, recoveries of 95 per cent silver, 98 per cent lead and 84 per cent zinc were obtained. The Investigation on the sample of ore, which was designated as "Sulphide Ore", showed that it responded readily to flotation concentration. Satisfactory grades and recoveries of copper, lead, and zinc were produced as indicated by the following summary of results from Test 43:

		Assay	s		I	Distrib	ution %	
Product	Ag oz/ton	Cu %	Pb %	Zn %	Ag	Cu	Pb	Zn
Cu conc Pb conc Zn conc	220.46 19.83 2.80	27.90 - -	8.30 67.00 4.01	12.20 9.36 58.19	38.8	55.8	1.1 82.4 11.2	0.8 6.0 86.3

The above results were obtained at a grind of 74 per cent minus 200 mesh. In other tests done at grind of 58 per cent minus 200 mesh, similar results were obtained (See Test 34). It is expected that a grind of 60 per cent minus 200 mesh would be sufficient for the liberation of the minerals in the sulphide sample.

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APPENDICES

APPENDIX A

INDUSTRIAL CONFIDENTIAL

MINERAL SCIENCES DIVISION

Internal Report MS 69-40

MINERALOGICAL EXAMINATION OF A HEAD SAMPLE OF LEAD-SILVER ORE FROM PRAIRIE CREEK, NORTHWEST TERRITORIES, ON BEHALF OF CADILLAC EXPLORATIONS LIMITED

by

D. R. Owens*

INTRODUCTION

A head sample of lead-silver ore from a deposit located on Prairie Creek, B. C., 210 miles north of Ft. Nelson and 110 miles west of Ft. Simpson, was received from Mr. A. Wall of the Mineral Processing Division on April 10, 1969. Mr. Wall stated that the ore had originally been submitted to the Mines Branch by the consulting mining engineer, Mr. K. V. Christie, 1310- 56th Street, Tsawwassen, Ladner, B. C., on behalf of Cadillac Explorations Limited, 570 Crown Trust Bldg., 407- 8th Avenue, Calgary 2, Alberta. Mr. Wall requested that the head sample be examined microscopically to identify its constituent minerals.

SAMPLE

The sample, as received, consisted of a portion of the head sample crushed to minus 10 mesh. The head sample was labelled No. 1 and was reported by Mr. Wall to contain 24.24% Pb, 1.79% Zn, 0.24% Cu, and 7.25

*Technical Officer, Mineralogy Section, Mineral Sciences Division, Mines Branch, Department of Energy, Mines and Resources Ottawa, Canada. ounces of silver per ton. It was also stated by Mr. Wall that the ore was reported to be contained in a quartz-carbonate matrix, throughout the shear zone, which is highly oxidized to a depth of at least 500 feet.

METHOD OF INVESTIGATION

The head sample was screened and the 48 to 65, 65 to 150 and 150 to 270-mesh fractions were removed. These fractions were each separated into a number of sink and float products by means of heavy liquids in order to concentrate the heavier ore minerals. The float products were analysed by Mr. E. J. Murray of the Crystal Structure Group by means of an X-ray diffractometer to identify the major gangue minerals. Polished sections were prepared from the sink products and examined microscopically to identify the heavier ore minerals. When corroboration of the identity of a mineral was necessary, samples were submitted to Mr. J. M. Stewart and Mr. E. J. Murray of the Structure Group for powder X-ray diffraction analysis.

RESULTS OF INVESTIGATION

General Mineralogy of the Head Sample

Since no hand specimens of the ore were available, the results of the examination are based solely on the head sample.

The examination of the head sample shows that the lead, zinc and copper occurs both as sulphides and as carbonates, and that the silver in the sample occurs as a constituent of argentiferous tetrahedrite. The leadbearing minerals are galena, bournonite, and cerussite; the zinc-bearing minerals are sphalerite and smithsonite; and the copper-bearing minerals are covellite, enargite, chalcopyrite and malachite. Also present in the head sample are pyrite, goethite, quartz, dolomite, pyroxene and an unidentified phase. Galena is the major metallic mineral in the head sample, with the other minerals occurring in much smaller amounts.

Detailed Mineralogy of the Head Sample

Lead-bearing minerals

The lead-bearing minerals are galena, cerrusite and bournonite, (PbCuSbS₃), with galena greatly predominating. Galena occurs mainly as free grains, but also to a minor degree as inclusions from about 5 to 70 microns in size in sphalerite, cerussite and gangue. (The word "size" as used in this report, refers to the greatest dimension of the mineral grain being described.) The galena itself contains few inclusions, and these are comprised of sphalerite, pyrite, covellite, bournonite and tetrahedrite.

The relatively small amount of cerussite in the sample is present as free grains and in association with galena and the other carbonates.

The amount of bournonite found in the sample is very small. It occurs as free grains, as inclusions in galena and gangue, and in combination and association with galena, tetrahedrite and enargite.

Zinc-bearing minerals

Only very small quantities of sphalerite and smithsonite are present in the head sample. The chief occurrence of the sphalerite is as free grains and in association with the galena, although some occurs as inclusions in gangue and in combination with covellite. Electron-probe microanalysis of the sphalerite shows that it has a low iron content (about one per cent or less).

The small amount of smithsonite present in the sample also occurs as free grains and in association with the other carbonates. The relative proportions of sphalerite and smithsonite are difficult to estimate because of the difficulty of distinguishing smithsonite from cerussite.

Copper-bearing minerals

The reported copper content of the head sample is quite low and therefore only very small amounts of copper-bearing minerals were seen. Chief amongst these is covellite, which occurs as inclusions in gangue and in association with sphalerite and galena. Minute amounts of enargite $[Cu_3(As, Sb)S_4]$ are present as free grains and as inclusions in tetrahedrite and gangue. Only traces of chalcopyrite and malachite were seen in the head sample. The chalcopyrite was observed as a number of minute grains in sphalerite, and malachite as a few free grains.

Silver-bearing minerals

Only one silver-bearing mineral was identified in the head sample. This is argentiferous tetrahedrite, containing about 1.3% silver as determined by electron-probe microanalysis. The tetrahedrite occurs as free grains, as inclusions in galena, and in association with bournonite and enargite.

Other ore minerals

The other ore minerals are pyrite and goethite. These occur in small amounts and are generally associated with each other, with the goethite veining or rimming about one half of the pyrite grains in the sample.

Gangue minerals

The gangue is composed essentially of quartz. Also present is a small quantity of dolomite and traces of pyroxene. A few grains of an unidentified mineral were also found in the float products of the head sample. X-ray diffraction studies of a few of these grains gave a powder pattern close to that of beudantite, which is a sulphate-arsenate of lead and ferric iron. This identity, however, could not be substantiated by the literature and its identification is therefore only tentative.

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CONCLUSIONS

The mineralogical examination of the head sample leads to the following conclusions: Galena is the major lead-bearing mineral, and also the major ore mineral. It is largely free from the other minerals in the sample, even in the 48 to 65-mesh fraction. Much less lead occurs as cerussite, which is also of a generally coarse grain size. Zinc, on the other hand, appears to be present in approximately equal amounts as a sulphide and as a carbonate. While some of the tetrahedrite is present as free grains, it is expected that a small proportion of it will present problems in liberation from the other minerals in the head sample. The very small amounts of copper-bearing minerals preclude an assessment of their liberation characteristics.

APPENDIX B

Test Report Data Sheets

Abbreviations used in Test Data Reports:

NaCN	Sodium Cyanide
$ZnSO_4$	Zinc Sulphate
CaO	Lime
A.31	Aerofloat Reagent 31
Z-11	Sodium Isopropyl Xanthate
404	Cyanamid Promoter 404
DF250	Dow Froth 250
$CuSO_4$	Copper Sulphate
SB	Sodium Bichromate
H_2SO_4	Sulphuric Acid
Z-200	Isopropyl ethyl thiono carbomate
Z-6	Potassium Amyl Xanthate
CA	Cresylic Acid
Ammo Phos	Ammonium Phosphate
Na_2SO_3	Sodium Sulphite
Na_2S	Sodium Sulphide
Na_2SiO_3	Sodium Silicate
3037	Aeromine 3037 Promoter
Z-5	Potassium sec amyl xanthate
PO	Pine Oil
444	Cyanamid Promoter 444
Z-8	Potassium sec butyl xanthate
Na_2CO_3	Sodium Carbonate
RM	Rod Mill

					on Sampl	e No.	1, Vei	n No. 3	, Zone	No.	3		TE: Apr ARGE:		969
OBJECT OF TEST Prelim	inary	flota	tion	test.	•								STED E		W.
	Time	%	Hq		Unit	Ι			Rea	gents,	lb p	er ton			·····
OFERATION	min	Solids	рп		used	A31	ZnSO4	NaCN	Z-11	CA	CuSC	4 Ča	0		
Grind (66.8%-200 m)	20	67	6.0	7 x	: 14 RM	0.04	0.40	0.20							-
Condition	2	45	7.0	100	0-g cell				0.10			1.	0		
Pb float	7	25	6.0			· · · · · ·	· · · · · · · · · · · · · · · · · · ·			0.03					
Zn condition	5	20	8.3		<u></u>						0.50	1.	0		
Zn float	6	20	6.7						0.10	0.03					
Pb clean	3			50	0-g cell										
Zn clean	2				0-g cell										
PRODUCT	W	11			1	YSIS		· · · ·				DISTR	IBUTIC		. <u>.</u>
_	%	<u> </u>		Ag	Pb N	.S.Pb	S. Pb	Zn	<u>Cu</u>	_		Ag	РЪ	Zn	Cu
Clean Pb conc Clean Pb tail	11	.0 .2	1	21.68 20.73	81.52 48.39			0.26 2.48	0.23 0.84	11		5 3. 1 16.5	62.6 12.1	2.6	18.5
Rough Pb conc (calcd)	21	•2		21.45	73.39		•	0.81	0.38			69.6	74.7	10.4	40.5
Clean Zn conc Clean Zn tail	11	•7 •0		12.54 7.96	24.00 18.63			3.11 3.27	0.80	. 11	-	5.2 4.9	3.6 3.6	5.1 7.9	11.0 9.0
Rougher Zn conc (calcd)	6	.7		9.80	22.28			3.21	0.60			10.1	7.2	13.0.	20.0
Bulk rough conc (calcd)	27	.9	1	L8.65	61.12			1.38	0.43			79.7	81.9	23.4	60.5
Rougher tail	72	•1		1.83	5.25.	4.83	0.42	1.89	0.11			20.3	18.1	76.6	39.5
Feed (calcd)	100	.0		6.53	20.80			1.65	0.20		1	00.00	100.0	100.0	100.0

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			_		on, Sam	ple No.	1, Vei	n No.3	, Zone	No.3		DAT	E: Apr	il 9, 1	.969
OBJECT OF TEST: Preli	iminar	v flota	ation	test										1000-g	
												·	TED E	3Y: W.A.	W.
OPERATION	Time	%	pН	-	Jnit				Rea	agents,	lb per	ton			
		Solids		L	used	A.31	ZnSO4	NaCN	<u>z-11</u>	Ca0	CuS04	CA			
Grind (53.7%-200 m)	15	67		7 x	14 RM	0.04	0.40	0.20							
Condition	2	45	8.5	1000	-g cell				0.10	1.00					_
Pb float	7	20	6.3									0.03			
Zn condition	5	20	9.9							1.00	0.50		_		
Zn float	6		9.0						0.10			0.03			
Pb clean	3				-g cell										
Zn clean	2	1		250	-g cell										
PRODUCT	W					LYSIS					DI	STRIE	BUTIO	N %	
	9	0		Ag	Pb	N.S.Pb	S. Pb	Zn	Cu			Ag	Pb	Zn	Cu
Clean Pb conc Clean Pb tail	12. 12.	14			80.50 58.50			0.57			43 30	.7 .9	45.5 32.6		24.9 26.8
Ro Pb conc (caled)	24	.5		19.66	69. 23			1.26	0.45		74	.6	78.1	14.2	51.7
Clean Zn conc Clean Zn tail	11	.1 .9			20.00 13.25			4.60 1.44		11		.7 .3	1.9 1.2		5.6 5.6
Ro Zn conc	4.	.0		8.21	16.80			3.10	0.60		5	.0	3.1	5.7	11.2
Bulk rough conc (calcd)	28	.5		18.06	61.87			1.52	0.47		79	.6	81.2	19.9	62.9
Rougher tail	71	.5		1.84	5.73	5.31	0.42	2.44	0.11		20	•4	18.8	80.1	37.1
Feed (calcd)				6.47	21.73			2.18	0.21		100	.0	100.0	100.0	100.0
REMARKS: * From Inte	rnal I	Reports	MS-A	C-69-0	406 and	453.									

Grind (53.7%-200 m)15Condition2Flotation9Condition5Flotation5Flotation2Photation12PRODUCTWPRODUCT%Clean Pb conc20.Clean Pb tail9.Ro Pb conc (calcd)29.Clean Zn conc1.	% Solid 67 45 25 25 20	Ha	7 x 1000	Unit Used 14 RM D-g cell D-g cell D-g cell D-g cell	A 31 0.04 0.01		ZnSO4 0.4	Rea CaO 1.0	0.10	1b per CuSO4 2.00	TEST ton CA	ED B	1000-g	
OPERATION min Grind (53.7%-200 m) 15 Condition 2 Flotation 9 Condition 5 Condition 5 Condition 5 Photon 12 PRODUCT W % 9 Clean Pb conc 20 Clean Pb tail 9 Co Pb conc (calcd) 29 Iean Zn conc 1	Solid 67 45 25 25 20 7	s 7.9 6.9	7 x 1000	used 14 RM D-g cel1 D-g cel1 D-g cel1	0.04	0.2		<u>Ca</u> 0 1.0	Z-11 0.10	CuSO4	ton CA			
minGrind (53.7%-200 m)15Condition2Flotation9Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Condition5Clean12Clean Pb conc20Clean Pb tail9Co Pb conc (calcd)29Clean Zn conc1	67 45 25 25 20	s 7.9 6.9	7 x 1000	used 14 RM D-g cel1 D-g cel1 D-g cel1	0.04	0.2		1.0	0.10					
Condition2Flotation9Condition5Condition5Flotation5Pb clean2Zn clean1½PRODUCTW%%Clean Pb conc20.Clean Pb tail9.Ro Pb conc (calcd)29.Clean Zn conc1.	45 25 25 20 T	6.9	500	9-g cell 9-g cell 9-g cell	0.01		0.4			2.00				
Flotation 9 Condition 5 Flotation 5 Flotation 2 Protect 2 In clean 1½ PRODUCT W 9 2 Clean Pb conc 20 Clean Pb tail 9 Ro Pb conc (calcd) 29 Clean Zn conc 1	25 25 20 T	6.9	500	-g cell				2.0		2.00				
Condition 5 Flotation 5 Flotation 5 Photes 2 Zn clean 1 ¹ / ₂ PRODUCT W PRODUCT % Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.	25 20	11.0	500	-g cell				2.0	0.05	2.00				
Flotation 5 Flotation 5 Phote 2 In clean 1½ PRODUCT W PRODUCT % Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.	20		500	-g cell				2.0	0.05	2.00				
Flotation 5 Pb clean 2 In clean 1½ PRODUCT W PRODUCT % Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean In Conc 1.	20		500	-g cell					0.05					
Zn clean1½PRODUCTW%%Clean Pb conc20.Clean Pb tail9.20 Pb conc (calcd)29.Clean Zn conc1.	11			-g cell				· · · ·						
PRODUCT W 9 Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.	11		250		Veis			· · · · · · · · · · · · · · · · · · ·						
PRODUCT W 9 Clean Pb conc 20. Clean Pb tail 9. Co Pb conc (calcd) 29. Clean Zn conc 1.	11										····	1		
PRODUCT % Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.	11	<u> </u>		ANAL		1					`	<u>+</u>		
Clean Pb conc 20. Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.	/6				-1212	%			<u> </u>	DI	STRIB		N %	
Clean Pb tail 9. Ro Pb conc (calcd) 29. Clean Zn conc 1.			Ag		.S.Pb	Zn	Cu				Ag	Рb	Zn	Cu
Ro Zn conc (calcd) 2. Rougher tail 68.	.1 .1 .6 .3 .9 .0		11.81 18.26 7.03 4.95 6.07 1.68	62.85 19.2 14.9 17.3 4.7	4.27	0.62 3.10 1.40 3.25 5.70 4.34 2.00	0.33 0.62 0.42 0.90 0.58 0.76 0.14				5.2 0.1 1.7 1.0 2.7 7.2	70.7 12.5 83.2 1.4 0.9 2.3 14.5	14.9 21.5 2.7 3.9 6.6 71.9	23. 51. 5. 3. 9. 39.
eed (calcd) 100.	·		6.63			1.89	0.24			100	0.0 1	0.00	100.0	100.
eed (assayed)	0		6.07	20.00	5.00	1.72	0.19							
ough bulk conc (calcd) 32	•0		17.16	58.82		1,66	0.45			82		35.5	28.1	60.

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			Explo	oratio	n Sampl	e No. 1	, Vein	No. 3,	Zone	No. 3	}		TE: Apr		
OBJECT OF TEST: Coar	rser Gr	ind											ARGE:		· · · · · · · · · · · · · · · · · · ·
		·····											STED B	Y: WAW	
OPERATION	Time	%	Hq		Jnit						, lb per				·
	min	Solids	·	L	ised	A. 31	ZnS04	NaCN	Ca0	Z-11	CuS04				
Grind (44.0%-200 m)	10	67		7 x 1	.4 RM et	0.04	0.40	0.20	1.0					_	
Condition	2	45	8.9	1000-	g cell				1.0	0.10		<u> </u>			
Pb float	7	25	6.9								1				
Zn condition	5	20	9.7						1.0		0.50				
Zn float	6		7.7							0.10					
Pb clean	3			500-	g cell										
<u>Zn clean</u>	1.5			250-	g cell										
PRODUCT	W.	1			ANAI	_YSIS	%* ·				DI	STR	IBUTIO	N %	
	%	6		Ag	РЪ	N.S.Pb	S. Pb	Zn	Cu			Ag	РЪ	Zn	Cu
Clean Pb conc	15	.6		20 70	75.32			0.66	0.2	2	5	4.8	59.0	6.1	23.7
Clean Pb tail	14	.7		12.03	34.00			2.69	0.4	13		5.6	13.1	12.1	18.3
Ro Pb conc (calcd)	23	.3		17.84	61.67			1.33	0.33	3	7	0.4	72.1	18.2	42.0
Clean Zn conc	3	.3		6.24	15.88			3.38	0.41			3.5	2.6	6.5	7.5
Clean Zn tail	2	.7		4.46	12.48			3.10	0.33	3		2.1	1.7	4.9	4.8
Ro Zn conc (calcd)	6	.0		5.95	14.35			3.25	0.38	3		5.6	4.3	11.4	12.3
Bulk ro conc (calcd)	29	.3		15.30	51.98			1.72	0.34	+	7	6.0	76.4	29.6	54.3
Rough tail	70	.7		2.00	6.50	4.51	1.99	1.70	0.12	2	2	4.0	23.6	70.4	45.7
Feed (calcd)	100	.0		5.90	19.92			1.70	0.19)	10	0.0	100.0	100.0	100.0
REMARKS: * From Inte	rnal R	eports	MS-A	C-69-4	406 and	4 48									

TEST NO. 8 SA	MPLE: (Cadillac	Expl	orati	on Sampl	e No. 1	l, Veir	n No.3	, Zone	e No. 3	3	DA	TE: Apr	il 30,	1970
OBJECT OF TEST: pH	control	. with s	odium	carb	onate							СН	ARGE:1	000-g	
												TE	STED B	Y: WAW	
OPERATION	Tim	1	нa		Unit			•		igents,					
	mir	Solids	р 5		used	A. 31	NaCO3	Z-11	CA	CaO	CuS04				
Grind (53.7%-200 m)	15	67		7 x	14 RM	0.06	1.0								
·····			ļ									<u> </u>			
Condition	3	45	7.2	100	D-g cell	·	3.0	0.10		 		ļ			
i			· .	· ·	·	_						<u> </u>			_
Pb float	6	25	6.7						0.03	1					
7n condition	5	20	10.6		······································			· · · · ·		1 00	1.00				
Zn condition			10.0							1.00	1.00				
Zn float	4	.20							0.03						
														_	
	I			<u> </u>											
PRODUCT	· \	VT			ANA	LYSIS	% *	-			D	ISTR	IBUTIO	N %	
		%		Cu	Pb	Zn					<u> </u> C	u	Pb	Zn	
Ro Pb.conc		1.4		0.56	72.00	0.85					5	2.9	74.0	10.3	
	- -			5.50	12.00	0.05						2.9	74.0	10.5	
Ro Zn conc		5.9		0.46	14.27	3.66					1	1.9	4.0	12.2	
Bulk conc (calcd)	2	7.3	0	0.54	59.52	1.46					6	4.8	78.0	22.5	
Rougher tail	7	2.7		0.11 [.]	6.27	1.89					3	5.2	22.0	77.5	
Feed (calcd)	10	0.0		0.23	20.81	1.77					10	0.0	100.0	100.0	
							•			ł.					
												1			
REMARKS: * From I	nternal	Report	MS-AC	-69-7	<u> </u> フク]. 	1					<u> </u>
REMARKS: " PION I		report	10-40	,	F1 44										
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	MPLE: Cad					e No. 1	, Vein	No. 3	, Zone	No. 3				il 30,	1970
OBJECT OF TEST: Rep	eat of 1	[est 8	at co	arser	grind									1000-g	
	·											<u> </u>		BY: WAW	
OPERATION	Time	%	рН	1	nit		· · · · · ·	1		agents,	· · · · · · · · · · · · · · · · · · ·	ton			
	min	Solids			sed			Z-11	Ca0	CuS04	CA				
<u>Grind (44.0%-200 m)</u>	10	67		7 x 1	.4 RM	0.06	1.0					ļ			
Condition	7	45	7.3	1000-	g cell		2.0	0.10							-
Pb float	7	25	6.7							· · · · · · · · · · · · · · · · · · ·	0.03				
Zn condition	5	20	10.8		· · · · · · · · · · · · · · · · · · ·				2.0	1.0					
Zn float	4	20	9.7								0.03				
Pb clean	$\frac{3}{1\frac{1}{2}}$				g cell	-									
Zn clean		<u> </u>		250-	g cell					<u> </u>		<u> </u>			
PRODUCT	W' %				· · · · · · · · · · · · · · · · · · ·	YSIS	% *						BUTIC	N %	
				Cu	РЪ	Zn						Cu	РЪ	Zn	
Clean Pb conc Clean Pb tail		.1		- 1	79 . 17 47.00	0 .6 2 2 . 28						3.0 3.5	56.7 14.5		
Ro Pb conc (calcd)	21	.6	0	0.43	69.49	1.12					4	6.5	71.2	13.7	
Clean Zn conc Clean Zn tail		•6 •4		0.41 0.44	10.98 12.12	3.29 2.63						3.5 5.5	0.8 1.4		
Ro Zn conc (calcd)	4	.0	0	0.45	11.70	2.90						9.0	2.2	6.6	
Bulk conc (calcd)	25	.6	0	0.43	60.46	1.40					5.	5.5	73.4	20.3	
Rougher tail	74	.4	0	.12	7.52	1.89					4	4.5	26.6	79.7	
Feed (calcd)	100	.0	c	.20	21.07	1.76					10	0.0	100.0	100.0	
REMARKS: * From Int	ernal R	eport 1	MS-AC-	69-47	2.			<u></u>	<u>.</u>	!	!	I			

			Expl	orati	on Samp	le No.	1, Vei	n No.3	, Zone	e No. 3	3			, 2, 196	59
OBJECT OF TEST: Pron	noter 4	404					、 、							1000-g	
	1											A	TED I	BY: WAV]
OPERATION	Time	%	pН	1	Jnit				······		, lb per				
	min	Solids			used	A. 31	ZnSO4	NaCN	Ca0	Z-11	404	CA	CuS	04	_
Grind (53.7%-200 m)	15	67	7.0	<u>7 x</u>	14 RM	0.04	0.4	0.2	1.0						
Condition	6	45	8.6	100	0-g cel	L			1.0	0.05	0.05		-		_
Pb float	7	25	7.1									0.02			
										İ	1				
Zn condition	-,5	25	10.1	<u> </u>			· ·		2.0	0.05			2.0	0	
Zn float	4	20	9.1							0.05					
Pb clean	2			500)-g cell										
Zn clean	1.5			1)-g cell					1					
PRODUCT	W-					YSIS	% *			1	DI	STRIB	UTIC	N %	
	%			Cu	Pb	Zn					(Cu	РЪ	Zn	1
Clean Pb conc	18.	6		0.37	79.35	0.52	•	、 、	1		2	9.7	67.4		
Clean Pb tail	5.	11	1	0.62	29.59	2.31					1	5.2	7.8	1	
Rough Pb conc (calcd)	24.	4		0.43	67.52	0.95					4	4.9	75.2	15.5	
Clean Zn conc Clean Zn tail	2.			0.73	17.50							7.2	1.9		
Stean all fait	3.	۲		دد.ر	15.14	2.41						7.2	2.2	5.2	
Rough Zn conc (calcd)	5.	6	(0.61	16.14	2.82					1	4.4	4.1	10.6	
Bulk conc (calcd)	30.	0		.47.	60.46	1.20					5	9.3	79.3	26.1	
Rougher tail	70.	o		.14	6.47	1.58					4(0.7	20.7	. 73.9	
eed (calcd)	100.	0	0	.24	21.91	1.50					100	0.0 1	00.0	100.0	

EMARKS: * From Internal Report MS-AC-69-512.

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					on Sampl	.e No.	l, Vei	n No.	3, Zon	e No.	3			y 2, 19	69
OBJECT OF TEST: PH	contro	l with	sodiu	m car	bonate									1000-g	
												_	TED E	3Y: WAW	·
OPERATION	Time	%	рΗ		Jnit			·	Rea	gents,	lb per	ton		····	
	min	Solids		1	used	A. 31	ZnS04	NaCN	Na ₂ CO ₃	404	Z-11	CuS	D_4 CaO		_
Grind (53.7%-200 m)	15	67		7 x	14 RM	0.04	0.40	0.20	1.0	0.05					
Condition	2	45	6.7	1000	-g cell				3.0		0.05				
Pb float	7	25	7.0												
Zn condition	5	25	10.4								0.05	2.00	2.0	0	
Zn float	4	20	9.9								0.10				
Pb_clean	2				-g cell										
Zn clean	1.5	<u> </u>	<u> </u>	250	-g cell	<u> </u>									
PRODUCT	W				ANAL	YSIS	<u>% *</u>				DI	STRI	BUTIC	N %	
	%	>		Cu	Pb	Zn					<u> </u>	<u>u</u>	РЪ	Zn	
Clean Pb conc Clean Pb tail	18. 7.			0.33 0.64	82.73 20.42	0.50 2.40					26 21	.3 .9	70.2 7.4	5.1 10.5	
Ro Pb conc (calcd)	25.	7		0.42	64.10	1.07					48	.2	77.6	15.6	
Clean Zn conc Clean Zn tail	4. 3.			0.50 0.42	12.17 12.35	4.31 2.96					10 5	.3 .8	2.7 1.7	11.2 5.1	
Ro Zn conc (calcd)	7.	6		0.47	12.25	3.77					16	.1	4.4	16.3	
Bulk conc (calcd)	33.	3		0.67	52.24	1.69					64	.3	82.0	31.9	
Rougher tail	66.	7		0.12	5.71	1.80					35	.7	18.0	68.1	
Feed (calcd)	100.	0		.22	21.82	1.76					100	.0 1	00.0	100.0	

REMARKS: * From Internal Report MS-AC-69-515.

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	MPLE: C			lorat	ion, Sam	ple No	. 1, Ve	ein No	. 3, Zo	ne No.	3	-	-	6, 197	0.
OBJECT OF TEST: Rep	peat of ?	rest 11	L											1000-g	
		,										<u> </u>	TED E	3Y: W.A	.W.
OPERATION	Time	%	рН		Unit		· · · · · · · · · · · · · · · · · · ·			igents,	·				
	min	Solids			used	A. 31	IZnSO4	NaCN	Na ₂ CO ₃	404	Z-1	L Cal) CuS	04 CA	
Grind (53.7%-200 m)	15	67		7 :	<u>x 14 RM</u>	0.04	0.4	0.20	1.0	0.10					
Condition	2	45	7.5	100	00-g cel	1			3.0		0.05				
Pb flotation	7	25	7.1					· · · · · · · · · · · · · · · · · · ·		 		 			
Zn condition	5	25	10.2	_							0.05	2.00	2.0	0	-
Zn float	4	20	9.4									<u> </u>		0.03	
Pb clean	2			25	50-g cell								·		
Zn clean	1.5			1	t <u>t</u> t										
PRODUCT	W.	τ			ANA	YSIS	%*		<u> </u>		D	STRI	BUTIO	N %	
	%	6		Cu	Pb	Zn		•				Cu	РЪ	Zn	
Clean Pb conc Clean Pb tail	16.	13		0.32 0.46	83.64 57.16	0.35 1.50						7.0 9.0	61.4 9.8		
to Pb conc (calcd)	20.	7		0.34	78.60	0;57					3	6.0	71.2	6.6	
llean Zn conc llean Zn tail	2.			1.51 0.69	37.59 19.39	8.24 1.56						6.0 7.0	3.4 2.0		
o Zn conc (calcd)	4.	4		1.05	28.07	4.75	•				. 2	3.0	5.4	11.7	
bulk conc (calcd)	25.	1		0.47	69.78	1.30	•				5	9.0	76.6	18.3	
ougher tail	74.	9		0.11	7.15	1.94					4	1.0	23.4	81.7	
eed (calcd)	100.	o II		0.20	22.87	1.78			· ·		10	0.0	100.0	100.0	

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EST NO. 13 SAMPLE: Cadillac Exploration, Sample No. 1, Vein No. 3, Zone No. 3													DATE: May 6, 1969			
OBJECT OF TEST: No sphalerite depression												CHARGE: 1000-g TESTED BY: W.A.W.				
OPERATION	Time	1	рН	Unit		Reagents, Ib per						- ton				
	min	Solids			Jsed	A. 31	Na2CO2	404	<u>z-11</u>	CuSO4	<u>Ca</u> 0	ļ				
Grind (53.7% - 200 m)	15	67		<u>7 x</u>	: 14 RM	0.04	1.0	0.10								
Condition	2	45	7.8	100	0-g cel:	1	3.0		0.05							
Pb floation	7	25	7.7			0.04										
Zn condition	5	20	10.5						0.05	2.0	2.0					
Zn floation	3	20	10.2													
Pb clean	2			50	0-g cel:	L										
Zn clean	1.5	<u> </u>		25	0-g cell											
PRODUCT	11	WT [,]			ANAL	YSIS %*					DISTRIBUTION %					
	%	6		Cu	РЪ	Zn						Cu	РЪ	Zn		
Clean Pb conc Clean Pb tail	17 6	•9 •8		0.35 0.54	81.19 31.55	0.56 2.75				an a		9.7 7.4	69.6 10.3	6.1 11.3		
Ro Pb conc (calcd)	24	•7	0	0.40	67.52	1.16					47	7.1	79.9	17.4		
Clean Zn conc Clean Zn tail		.4 .6	1).60).42		3.01 2.88						8.8 5.2	0.9 1.3	2.5 4.5		
Ro Zn conc (calcd)	4	.0	C	.48	11.50	2.92					ç	9.0	2.2	7.0		
Bulk conc (calcd)	28	.7	C	.41	59.70	1.42					56	5.1	82.1	24.4		
Rougher tail	71	.3	c	.13	5.26	1.75					43	.9	17.9	75.6		
Feed (calcd)	100	.0	c	.21	20.89	1.65					100	0.0	100.0	100.0		

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REMARKS: * From Internal Report MS-AC-69-538

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TEST NO. 14 SAMP	'LE: _{Ca}	dillac	Expl	oratio	n Sampl	e No. 1	., Vein	No. 3	, Zone	No. 3	1		TE: May		9
OBJECT OF TEST: Tabli	ng											CH	ARGE:	2000-g	
												TE	STED E	3Y: W.A.	W.
OPERATION	Time	%	Hq	1	Jnit				Rea	gents	lb p	er ton			
	min	Solids	P11		used										
Grind (1)									·						
Wilfley Table		ļ													
		· · · · · · · · · · · · · · · · · · ·			· · · · · · · · · · · · · · · · · · ·						ļ				
				·							ļ				_
					<u> </u>										
				_		•									
											· · ·				
PRODUCT	W	T·			ANA	LYSIS	% *	*		1	1	DISTR	RIBUTIC	N %	
FRODUCT	9	6		РЪ	NS: Pb	S.Pb	Zn				1	РЪ	NS.Pb	S.Pb	Zn
Table conc	19	.7		81.16	13.71	67.45	0.67					71.6	48.0	79.5	7.7
Table midd.	13	.7		25.66	14.02	11.64	8.04					15.7	34.1	9.5	64.1
Table tail (calcd)	66	.6		4.26	1.51	2.75	0.72					12.7	17.9	11.0	28.2
Feed (calcd)	100	.0		23.34	5.63	16.71	1.72	•			1	00.0	100.0	100.0	100.0
Conc + Midd (calcd)	33	•4		58.31	13.81	44.50	3.69					87.3	82.1	89.0	71.8
				:					1						
								-							
REMARKS: * From Inter	nal R	eport]	MS-A	C-69-54	<u>4</u> 4										
(1) Stage gr	ound	to min	us 6.	5 mesh							•				

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TEST NO. 15 SA	MPLE: Ca	dilla	c Expl	loratic	n Sampl	e No.	l, Veir	No.	3, Zone	No. 3	5	DA	TE: May	14, 19	969
OBJECT OF TEST: A	ffect of	Reage	nt 404	4 and A	mmonium	Phosp	nate						ARGE:		
									-			<u> </u>	STED B	Y: W.A.	.W.
OPERATION	Time		рН	1	Jnit				Rea	gents,	ib per	r ton			
	min	Solid	s	<u> </u>	sed	Ammo Phos	404	A31	CuS04	Ca0	Z-11				
Grind (66.8%-200 m)	20	67		<u>7 x</u>	14 RM	4,0									
Condition	1	45	7.	1 1000)-g cell		0.1								
Float	12	25	7.(2			0.4	0.04							
Condition	3	25	10.0	5					2.0	2.5	0.06				
Float	3	20	10.4	4											
						<u> </u>									
PRODUCT	11	'Τ			ANAL	YSIS	% *		·····		D	ISTR	IBUTIO	N %	
		%	Pb I	NS.Pb	_S.Pb		Zn	NS. Z	n S.Z	n Pł) NS	Pb	S. Pb	Zn	N.S.ZI
Ro Pb conc	3	5.0 5	8.90	14.00	44.90		1.60	1.19	0.41	95.	.7 8	8.6	98.2	33.6	28.0
Ro Zn conc		3.4	9.05	5.13	3.92		3.83	3.57	0.26	1.	.4	3.1	0.8	7.6	7.9
Bulk conc (calcd)	39	9.4 5	4.60	13.23	41.37		1.79	1.39	0.40	97.	.1 9	1.7	99.0	41.2	35.9
Rougher tail	60	0.6	1.06	0.78	0.28		1.66	1.62	0.04	2.	.9	8.3	1.0	58.8	64.1
Feed (calcd)	100	0.0 2	2.15	5.68	16.47		1.71	1.53	0.18	100.	0 10	0.0	100.0	100.0	100.0
												;			
REMARKS: * From In	l	eport	MS-AC	-69-54	<u> </u>				<u> </u>				l	<u> </u>	I
			110	J)-J4.											

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TEST NO. 16 SAMP	LE: Ca	adillad	$\mathbf{E} \mathbf{E} \mathbf{x}_{\mathbf{j}}$	plorati	ion Samp	ole No.	1, Vei	n No.	3, Zor	ne No	3	DA	TE: Jun	e 13, 1	1969
OBJECT OF TEST: Repe	at of	Tablin	ng T	est No.	. 14						-		ARGE:		
												TE	STED E	3Y: W.A.	.W
OPERATION	Time		pН		Unit				Rea	igents,	lb per	ton	· · · · ·		
	min	Solids	- · · q		used										
Grind (1)															
Wilfley Table															
				<u> </u>											
-						•				<u> </u>					
		·									****				
										<u> </u>	· · · · · · · · · · · · · · · · · · ·				
								-		•• .					
			· · · · · ·			-				· ·					
								· · · · ·							
DDODUOT	W	<u></u> Τ			ANA	LYSIS	<u></u> % *	!		1 1	DI	STR		N %	
PRODUCT	%	5		Рb	NS.Pb	S.Pb	Zn					?b	NS.Pb	S.Pb	Zn
Table conc	16	•3		80.11	12.31	67.80	0.30				65	5.0	39.3	73.7	3.0
Table midd.	18	•4		21.58	10.87	10.71	6.0				19	. 8	39.2	13.2	66.6
Combined conc-midd (calcd)	34.	.7		49.07	11.55	37.52	. 3.31				- 84	••8	78.5	86.9	69.6
Table tail	65.	.3		4.69	1.68	3.01	0.77				15	5.2.	21.5	13.1	30.4
Feed (calcd)	100.	.0		20.09	5.10	14.99	1.65				100	0.0	100.0	100.0	100.0
								·							
								•							
									<u> </u>						<u> </u>
REMARKS: * From Inte (1) Stag	rnal F e grov	Report ind to	MS-A minu	AC-69-5 1s 65 m	199 Jesh										
											· .				

OBJECT OF TEST: Impro	vemen	t of s	sphale	erite f	lotatio	n						CHAF	RGE: 1	000-e	
OPERATION											ł				
OPERATION													ED B	Y: W.A.	N
OFLIGATION	Time	%	На	<u>ι</u>	Init				Rea	igents,	lb per	ton			
	min	Solids		L	Ised	NaCN	ZnS04	Ca0	404	<u>Z-11</u>	la2C031	Na <u>2Si</u> O	3 Na2	s <u>3037</u>	
Grind (53.7% - 200 M)	15	67		<u>7 x</u>	14 RM								1 1		
Condition	5	45	7.3	1000)-g cel	1 0.2	0.4	1.0	0.5				-		
Flotation	6	25								0.10					
Condition	10	25	11.5								2.0	2.0	10.0	0.5	
Flotation	6	25													
Pb Clean	2		<u> </u>)-g cel								-		
Zn Clean	1		1	250	0-g cel:					<u> </u>					
PRODUCT	W .	12		4 - (1		LYSIS Zn	% *	[1		····		Pb	Zn	
					<u>)</u> Pb				-			g			
Clean Pb conc Clean Pb tail	25 21	64		19.31 4.16		1.02 2.40							79.3 13.1	15.0 30.3	
Ro Pb conc	47	•1		12.33	43.11	1.65					87	•7	92.4	45.3	
Clean Zn conc Clean Zn tail		•5 •6		7.56 2.48	18 .77 4.43							.3	4.7 0.9	34.4	
Ro Zn conc (calcd)	10	•1		5.25	12.18	6.66					8	.0	5.6	38.6	
Bulk conc (calcd)	57	•2		11.1	37.7	2.50					95	.7	98.0	83.9	
Rougher tail	42	.8		0.67	1.00	0.65					4	.3	2.0	16.1	
Feed (calcd)	100	.0		6.63	21.97	1.72					100	.0 1	00.0	100.0	

TEST NO. 18 SAMP	LE: Ca	dillac	Explo	oratio	on Sampl	e No.	1 <u>, Vei</u>	n No.	3, Zone	No.	3	DAT	E: Jur	e 26, 1	L969
OBJECT OF TEST: Diffe	erent	reagen	it comb	oinati	ion			•						000-g	1.7
			1	1		· · · ·							IEDE	Y: W.A	• W •
OPERATION	Time	%	рН		Jnit Jsed	Anno		1.1.0.1			lb per				
		Solids				Phos_	Ca0	404	A. 31	Na ₂ CO:	CuS04	Na ₂ S	303	7	
<u>Grind (53.7%-200 m)</u>	15	67		7 3	< 14 RM										
Condition	10	45	8.8	100	00-g cel	4.0	2.0	0.10	0.02						
D1 C1							<u> </u>								_
Pb flotation	11	25	<u> </u>					0.04							
Zn condition	10	- 25	11.7							4.0	2.0	15.0	0.2	0	
Zn flotation	5	25											0.2	0	
														×	
Pb clean	1.5				i	· · ·									
Zn clean	1.5					I	l	<u> </u>					<u> </u>		·
PRODUCT	W					YSIS					DI	STRIE	υτιο	N %	
·	%		· · · ·	$Ag^{(1)}$	РЪ	Zn		<u> </u>			A	g	Pb	Zn	
Clean Pb conc Clean Pb tail	17 3	.8 .8		3.33 4.03	82.86 35.17	0.60 2.81	·				1	.3	78.1 7.1	10.7 10.6	
Ro Pb conc (calcd)	21	.6	2	1.69	74.47	0.99					73	.7	85.2	21.3	
Clean Zn conc Clean Zn tail	13	.2		1.02 8.51	33.68 24.97	9.13 4.55						.1	2.1 4.1	10.9 14.0	
Ro Zn conc (calcd)	4.	.3		9.21	27.40	5.84					6	•2	6.2	24.9	
Bulk rougher conc (calcd) 25	.9	1	9.62	66.65	1.80					79	.9	91.4	46.2	
Rougher tail	74.	.1		1.73	2.20	0.73					20	.1	8.6	53.8	
Feed (calcd)	100.	0	(6.36	18.89	1.00					100	.0 10	0.00	100.0	
REMARKS: * From Int (1) ounces			ts MS-	AC-69	-591 and	1 625		<u> </u>	· · ·			· · ·			

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MINES BRANCH	FLOTATION	TEST REPORT
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TEST NO. 19 SAMP	PLE: (Cadilla	c Exp	lorat:	ion Sampi	Le No.	1, Vei	in No.	3, Zo	ne No.	3	DAT	E: July	77,19	69
OBJECT OF TEST: Repe	at Tes	t 18 a	t fin	er gri	ind					-		СНА	RGE: 1	.000-g	
L .												TES	TED B	Y: W.A.	W
OPERATION	Time	%	Hq	ι	Jnit				Re	agents,	lb per	ton			
	min	Solids			Jsed	Ammo Phos	404	A.31	Ca0	CuSO4	Na ₂ S	303	7		
Grind (66.8%-200 m)	20	67		7 :	x 14 RM										
Condition	10	45	7.0	100	00-g cel1	4.0	0.10								
Pb flotation	12	25	7.0				0.40	0.04							
Zn condition	3	25	11.1						4.5	2.0	15.0	0.2			
Zn flotation	5	25	11.5									0.2			
Pb_clean	2														
Zn clean	1.5	<u> </u>													
PRODUCT	W	1			ANAL	YSIS	% *		<u>.</u>		DIS	STRI	SUTIO	v %	
	9	<u> </u>		РЪ	Zn							?Ъ	Zn		
Clean Pb conc Clean Pb tail	25 6	.9 .7	1	6.25 27.68	0.48 2.75						80 8		7.5		
Ro Pb conc (calcd)	32	.6	5	58.30	0.94						89.	.3	18.6		
Clean Zn conc Clean Zn tail		•2 •1		25.12	2.46 2.44						1	.8	4.7 7.4		
Ro Zn conc (calcd)	8	.3	1	.8 .3 0	2.45		·				7.	.2	12.1		
Bulk rough conc (calcd)	40	.9	5	50.20	1.25						96.	.5	30.7		
Rough tail	59	•1		1.30	1.95						3.	.5	69.3		
Feed (calcd)	100	.0	2	1.31	1.66						100.	0 1	00.0		
REMARKS: * From Inte	ernal I	Report	MS-AC	-69-6	25.		<u></u>								

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OPERATIONTime min% SolidsGrind $(66.8\%-200 \text{ m})^{(1)}$ 2067Condition545Pb flotation925Deslime	pH Unit used 7 x 14 RM 2000-g cell 6.8	Ammo Phos 404 A. 31 4.0	Reagents, 1b per CaO CuSO4 Na2S	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	ds P ^{FT} used 7 x 14 RM 2000-g ce11	Phos 404 A. 31		r ton
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	ds P ^{FT} used 7 x 14 RM 2000-g ce11	Phos 404 A. 31		
min Solids Grind (66.8%-200 m) ⁽¹⁾ 20 67 Condition 5 45 Pb flotation 9 25 Deslime (2) Zn condition 10 40 Zn flotation 7 25 Production 10 40 Zn flotation 7 25 PRODUCT WT PRODUCT WT Clean 2 Clean Pb conc 22.5 Clean Pb conc (calcd) 36.2 Clean Zn conc 1.2 Clean Zn conc (calcd) 4.3 Bulk rough conc (calcd) 40.5 Slime 7.5	is used 7 x 14 RM 2000-g cell	Phos 404 A. 31	CaO CuSO4 Na2S	
Condition545Pb flotation925Deslime (2)Zn condition1040Zn flotation725Zn flotation725Pb clean2Zn clean1.5PRODUCTWT%Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn conc (calcd)40.5Bulk rough conc (calcd)40.5Slime7.5	7 x 14 RM 2000-g cell			3037
Pb flotation925Deslime (2)Zn condition10Zn flotation7Zn flotation7Pb clean2Zn clean1.5PRODUCTWT%Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn conc (calcd)40.5Bulk rough conc (calcd)40.5Slime7.5				
Deslime(2)Zn condition10Zn condition10Zn flotation7Zn flotation7Pb clean2Zn clean1.5PRODUCTWT%%Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn conc (calcd)40.5Bulk rough conc (calcd)40.5Slime7.5	6.8	0.1		
Zn condition 10 40 1 Zn flotation 7 25 1 Zn flotation 7 25 1 Pb clean 2 2 2 Zn clean 1.5 1 1 PRODUCT WT % 1 Clean Pb conc 22.5 1 13.7 Glean Pb tail 13.7 36.2 1 Clean Zn conc 1.2 3.1 1 Clean Zn conc 1.2 3.1 1 Glean Zn conc (calcd) 40.5 3 1 Bulk rough conc (calcd) 40.5 7.5 5		0.4 0.04		
Zn condition 10 40 1 Zn flotation 7 25 1 Zn flotation 7 25 1 Pb clean 2 2 2 Zn clean 1.5 1 1 PRODUCT WT % 1 Clean Pb conc 22.5 1 13.7 Glean Pb tail 13.7 36.2 1 Clean Zn conc 1.2 3.1 1 Clean Zn conc 1.2 3.1 1 Glean Zn conc (calcd) 40.5 3 1 Bulk rough conc (calcd) 40.5 7.5 5				
Pb clean2Zn clean1.5PRODUCTWT %Official Pb conc22.5Clean Pb tail Rough Pb conc (calcd)13.7Rough Pb conc (calcd)36.2Clean Zn conc Clean Zn tail Rough Zn conc (calcd)1.2Slime7.5	11.5		4.0 2.0 8.0	0.2
Pb clean2Zn clean1.5PRODUCTWT %Official Pb conc22.5Clean Pb tail Rough Pb conc (calcd)13.7Rough Pb conc (calcd)36.2Clean Zn conc Clean Zn tail Rough Zn conc (calcd)1.2Slime7.5	11.9			0.2
Zn clean1.5PRODUCTWT %Clean Pb conc Clean Pb tail Rough Pb conc (calcd)22.5 13.7 36.2Clean Zn conc Clean Zn tail Rough Zn conc (calcd)1.2 3.1 4.3Bulk rough conc (calcd)40.5 7.5				
PRODUCTWT %Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	500-g cel1			
PRODUCT%Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	<u> </u>			
Clean Pb conc22.5Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	1	′SIS % *		ISTRIBUTION %
Clean Pb tail13.7Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	Pb Zn			Pb Zn
Rough Pb conc (calcd)36.2Clean Zn conc1.2Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	73.25 0.91		1 11 1	78.2 11.0
Clean Zn conc Clean Zn tail Rough Zn conc (calcd) Bulk rough conc (calcd) Slime 1.2 3.1 4.3 40.5 7.5	26.50 2.80		1 11	17.2 20.7
Clean Zn tail3.1Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	55.55 1.63		S	95.4 31.7
Rough Zn conc (calcd)4.3Bulk rough conc (calcd)40.5Slime7.5	12.68 5.17			0.7 3.3
Bulk rough conc (calcd) 40.5 Slime 7.5	4.22 2.45			0.7 4.1
Slime 7.5	7.07 3.20			1.4 7.4
	50.41 1.80		g g	96.8 39.1
Pouchon tot $\ 520 \ $	3.91 2.19			1 4 8.8
	0.71 1.86			1.8 52.1
Feed (calcd) 100.0	21.07 1.86		10	0.0 100.0
REMARKS: * From Internal Report M (1) Ground in 2 1000-gram batch				<u></u>

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TEST NO. 21 SAM	PLE: Ca	dillac	Expl	oratio	n Sampl	e No.	2, Lot	s 32, 3	33 & 3	4	<u></u>			. 15, 3	L969
OBJECT OF TEST: 0x	ide flo	tation	L									· · · · · · · · · · · · · · · · · · ·	RGE: 1		
													ED BY	: W.A.I	₹.
OPERATION	Time	%	pН	1	Jnit	Ammo.		+	Rea	agents,	lb per	ton	· • • • • • • • • • • • • • • • • • • •		
	min	Solids	P	<u> </u>	ised	Phos	404	ZnS04	A. 31	Na2CO2	<u>Na2SiO</u>	3 Na ₂ S	3037	DF250	
Grind (66.8%-200 m)	20	67		7 x	14 RM	4.0									
Condition	5	45	7.3	1000	-g cell		0.25	0.10							
Pb flotation	7.5	25					0.125	5	0.04	•					
Zn condition	10	25	10.9							4.0	3.0	15.0	0.25	0.03	
Zn flotation	4.5								 				0.25	0.04	
Ph clean	3			1	-g cell -g cell										
Zn clean	w	<u> </u>		1 300		YSIS	0/ *	1	I	<u>I. </u>		STRIB	UTION	1 <u>°6</u>	
PRODUCT	9			Рb	Zn	.1010	/0	1				Ъ			
													Zn		
Clean Pb conc Clean Pb tail	9 24	.4 .0		9.39 9.47	11.95 18.94							.8	6.4 25.8		
Clean Zn conc Clean Zn tail	29 12	11		4.87	28.25 8.71								+6.8 6.2		
Rougher tail	24		İ		10.42								4.8		
Feed	100				17.58										
reeu			Ľ	0.39	17.30						100	.0 10	0.0		
REMARKS: * From Ir	ternal	Report	MS-A	C-69-7	721		· · · · · · · · · · · · · · · · · · ·		· · · · · · · · · · · · · · · · · · ·						

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TEST NO. 22 SAN	1PLE: Ca	dillac	Explc	ratio	n Sampl	e No.	2, Lots	32, 3	33, & 3	34	······································	DAT	E: _{Sept} RGE:	. 23, 1000-g	1969
OBJECT OF TEST: Rep	eat of	Test N	0.21	at co	arser g	rind								<u> 1000 g</u> Y: W.	
OPERATION	Time	%	рН	1	Jnit	Ammo			Rea	igents,	lb per	ton	· · · · · · · · · · · · · · · · · · ·		
	min	Solids		. L	ised	Phos	404-	<u>z-11</u>	A.31_	Na 2CO	Na2SiC	Cuso	Na2S-	3037	DF250
Grind (53.7%-200 m)	15	67		7 x	<u>14 RM</u>	4.0	· · · · · · · · · · · · · · · · · · ·					1			
Condition	5	45	7.4	1000	-g cell		0.40								<u> </u>
Pb flotation	12	25		 			0.20	0.1	0.04				4.0		
Zn condition	10	25	·			4.0				6.0	3.0	1.0)		<u> </u>
Zn flotation	8	25	11.0				\			· · · · · ·			15.0	0.60	0.03
No. 1 Zn clean	2				-g cell										
No. 2 Zn clean		<u> </u>	<u> </u>	250	<u>-g cell</u>	1	0.4 sh			<u> </u>	<u> </u>			1	1
PRODUCT	W %	11		РЪ	Zn	YSIS	% ~					2b	Zn	<u> </u>	
Ro Pb conc	47	.7	4	2.10	13.24						89	9.1	33.3		
Cl Zn conc Cl Zn tail Recl Zn tail	13	•4 •9 •4	· .	2.63 2.83 6.92	37.20 32.80 40.00			- -			1	.7	12.5 24.1 17.7		
Ro Żn conc (calcd)	28	.7		6.21	35.89						7	.9	54.3		
Ro tail	23	.6		2.91	10.00						3	.0	12.4		
Feed (calcd)	100	.0	2	2.55	18.98						100	0.0 1	00.0		
							:								-
REMARKS: * From Int	ernal I	Report	MS-AC	-69-73	31.	<u>_</u>				<u></u>					
								•							

				ratio	on Sampl	e No.	2, Lots	32,	33 and	1 34				. 24,	1969
OBJECT OF TEST: Pb-2	Zn sepa	ration	L											000-g	
	1		1									[ED B	Y: W.A.	W .
OPERATION	Time	1	рН		Jnit used	Anno -	1		······		lb per			1	
		Solids				Phos	404	ZnS04	A.31	<u>Z-11</u>	Na ₂ CO ₂	Na ₂ Si	Na ₂ S	3037	DF250
Grind (53.7%-200 m)	15	67		7 x	14 RM	4.0					 				
Condition	5	45		1000)-g cell	1	0.25	0.20		0.10					
Pb flotation	10	25	7.5				0.20		0.02						
Zn condition	10	25									4.0	6.0			
Zn flotation	5	25	11.0										15.0	0.30	0.015
Pb clean	2			250	-g cell										-
Zn_clean	1.5	<u> </u>	<u> </u>	250	-g cell				<u> </u>						
PRODUCT	W %	- 11.			···· ··· ··· ··· ··· ··· ··· ··· ·	YSIS	% *							J %	
				Pb	Zn				-	_		b .	Zn		
Clean Pb conc	17	.8	4	5.05	11.92						37	.1	11.5		
Clean Pb tail	12	.5	2	8.47	16.44								11.1		
Rough Pb conc (calcd)	30	.3	3	8.21	13.79						53	.6	22.6		
Clean Zn conc	22	.5	2	7.04	25.44						28	.2	30.9		
Clean Zn tail	17		1	0.89	27.63								25.9		
Rough Zn conc (calcd)	39	.9	2	0.00	26.40						37	.0	56.8		
Rougher tail	29	.8		6.80	12.84						9	•4 2	20.6		
Feed (calcd)	100	•0	2	1.58	18.54						100	.0 10	0.0		
															1
REMARKS: * From Inte		enort N	<u>15-AC-</u>	69-73	3										
				U1-1U	~•										
			·····		·	·····							<u></u>		

TEST NO. 24 SAM	IPLE: C	adilla	Expl	orati	on Samp	Le No.	2, Lot	ts 32,	33 and	1 34			TE: Oct		
OBJECT OF TEST: Pb.	-Zn sepa	aation											ARGE:		
			<u></u>					<u>.</u>				· ·	TED BY	<u>: W.A</u>	W.
OPERATION	Time	%	На		Unit	Ammo			Rea	agents,	lb per	ton			
	min	Solids			used	Phos		CuS04	Na ₂ S	404	Z-5	Na ₂ C	03Na2SiC	3037	DF250
Grind (53.7%-200 m)	15	67		7 x	14 RM	4.0(1	P					! 			
Condition	5	45	7.5	1000	-g cell		0.04	2.0							
Pb flotation	11	25	· · · · · · · · · · · · · · · · · · ·	<u> </u>			0.04		0.3	0.25	0.25				
Zn condition	10	25	9.8			4.0		1.5				6.	0 9.0		
Zn flotation	10	25	9.8		<u>·</u>				17.0	· · · ·		 	· · · · · · · · · · · · · · · · · · ·	0.30	0.03
Pb. clean	2.5		, ,		· ·										
Zn clean	2.5														
PRODUCT	W	[1	···-		ANAL	YSIS	%*				DI	STRI	BUTION	1 %	
	%			РЪ	Zn							РЪ	Zn		
Clean Pb conc Clean Pb tail Rough Pb conc (calcd)	18. 27. 45.	.4	2	2.28 7.84 3.58	12.90 18.23 16.11						35	5.6 5.4 0	12.5 26.8 39.3		
Clean Zn conc Clean Zn tail Rough Zn conc (calcd)	15. 21. 36.	.1		2.12 4.00 6.00	22.63 26.85 25.05				•		3	3.4 3.9 7.3	19.0 30.4 49.4		
Rougher tail	17.	7		2.08	11.95						1	7	11.3		
Feed (calcd)	100.	0	2	1.54	18.66						100	.0	100.0		
REMARKS: * From Int (1) Additional reagent	eranl I s added	Report d to gr	MS-AC ind Z	-69-7 nS04	49 = 0.80 a	and NaC	N 0.20	1) 1b/to)n.			l			

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	PLE: Ca	adillac	: Expl	orati	on Sampl	e No.	2, Lot	s 32, :	33 and	34		DATE	UCL	. 17, 19	269
DBJECT OF TEST: P	b-Zn Se	eparati	lon at	fine	grind						:	CHAF		<u>1000-g</u>	
	1	T	T		<u>.</u>	<u>1</u>					lb per		ED BY	: W.A.W.	·
OPERATION	Time	% Solids	рН	1	Jnit Jsed	Ammo	404		r	·	· · · · · · · · · · · · · · · · · · ·		0.007	10000	
rind (approx. 75%-200m		67			14 RM	Phos 4.0	404	<u>Z-5</u>	A.31	Naguug	Na 25103	Na ₂ S	3037	DF250	
rind (approx: 75%-200m		07		\uparrow	14 101	4.0									<u>_</u>
Condition	5	45		1000	-g cell		0.25	0.10	0.04						
b_flotation	5	25	7.2				0.13				 				
In condition	10	25	10.9							4.0	6.0	15.0	0.25	0.03	
n flotation	7	25											0.25		
													<u> </u>		
PRODUCT	W				ANAL	YSIS	% *	,			DI	STRIB	UTION	%	
		6		Pb	Zn						<u>E</u>	Ъ	Zn		<u> </u>
lead conc	31	.1	12	38.60	13.93						56	5.3	23.1		
inc conc	29	.8		25.18	21.75						35	.2 3	34.6		
ougher tail	39	.1		4.61	2 0. 20						8	.5 4	42.3		
eed (calcd)	100	.0		21.31	18.71						100	.0 10	0.0		
										22 22 22 22 22 22 22 22 22 22 22 22 22					
REMARKS: * From Inte	ernal R	eport	MS-AC	-69-75	6.										

TEST NO. 26 SAMPLE: Cadillac Exploration Sample No. 2, Lots 32, 33 and 34 DATE: Oct. 17, 1969 CHARGE: 1000-g OBJECT OF TEST: Pb-Zn separation at coarse grind TESTED BY: W.A.W. Reagents, lb per ton Time % Unit Ammo OPERATION pН used Phos CuSO₄ A.31 404 Z-5 Na₂S Na₂CO_B 3037 DF250 min Solids 4.0¹) Grind (44%-200 m) 7 x 14 RM 10 67 Condition 5 45 7.5 <u>1000-g cell</u> 2.0 0.04 0.20 0.05 0.25 0.30 Pb flotation 0.3 10 25 25 9.4 4.0 6.0 Zn condition 10 Zn flotation 15.0 7 25 0.03 . 0.60 ANALYSIS % * WT DISTRIBUTION % PRODUCT % РЪ Zn РЪ Zn Lead conc 49.3 32.92 16.25 75.7 43.7 12.08 Zinc conc 2.5 15.48 1.8 1.6 Rougher tail 48.2 10.00 20.78 22.5 54.7 Feed (calcd) 100.0 18.33 21.44 100.0 100.0 REMARKS: * From Internal Report MS-AC-69-756 1) Additional Reagents to grind ZnS04-0.80, and NaCN-0.20 1b/ton

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TEST NO. 27 SAN	IPLE: Ca	dillac	Exp1c	ratic	n - Sul	phide (Ore					DA	TE: NOV	7.5,19	69
OBJECT OF TEST; P	relimina	ary te	st											1000-g	
			1							<u> </u>			STED E	3Y: W.A	• W •
OPERATION	Time	%	рН	1	Jnit used		10.11	1.01	· · · · · ·	igents,	,	· · · · · · · · · · · · · · · · · · ·	+ 70 C	0	
		Solids 67			· · · · · · ·	CaO	Z-11	404	A.31	CA	CuS04	Ca0	DF25	0	
Grind (74.5%-200 m)	1.5	67			14 RM										
Condition	5	45	7.5	100	0-g cel:	1 1.0	0.1	0.04	0.04						
Pb float	6	30	7.5			_				0.03					
Zn condition	10		10.5				0.05				2.0	2.0	<u></u>		
Zn float	3	30	10.5				0.05				2.0	2.0	0.0	3	
Pb Conc Clean	2			50	0-g cel1										
		<u> </u>													
PRODUCT	₩ ⁻ %	т			· · · · · · · · · · · · · · · · · · ·	LYSIS			-1		DI	r	BUTIC	DN %	r
		<u></u>	Ag (1)	Cu	РЪ	N.S.Pb	Zn	N.S.Z	n		<u>g</u>	Cu	Pb	Zn	
C1 Pb conc	36.			2.06	36.92		32.36			79	.1 7	8.9	84.7	38.8	
Cl Pb tail	36.	6 3	8.86	0.36	4.09		44.10			14	.3 1	4.0	9.5	53.5	
Ro Pb conc (calcd)	72.	8 12	2.64	1.22	20.40		38.30			93	.4 9	2.9	94.2	92.3	
Zinc conc	5.	0 7	.14	0.32	9.90		29.12			3.	.6	1.7	3.1	4.8	
Ro tail	22.	2 1	. 32	0.23	1.93		3.92			3.	.0	5.4	2.7	2.9	
Feed (calcd) Feed (assay)	100.			0.94 1.00	15.79 17.40	1.94	30 .1 8 30 . 80	1.14		100.	.0 10	0.0	100.0	100.0	
REMARKS: * From In	ternal	Report	MS - A	<u>-69</u> -	779 78/	and 8	 22		<u> </u>					<u> </u>	
	ince per		110 - A	0-09-	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	r ann 0	<i>~ L</i> •								
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TEST NO. 28 SAMP	LE: Ca	dillac	Expl	orati	on - Sul	.phide	Dre	<u></u>						$\frac{5v. 6, 1}{1000}$.969
DBJECT OF TEST: Prel	iminar	у кеад	ent l	nvest	igation			·						1000-g	T7
													TEDE	3Y: W.A.	W .
OPERATION	-Time	%	pН	1	Jnit	Ammo		1.01		gents,					
		Solids		+	used	Phos	Z-11	404	A.31	CA	CaO	CuSO	·		<u></u>
Grind (74.5%-200 m)	15	67		<u>7 x</u>	14 RM	4.0									
Condition	5	45	8.1	100	0-g cell		0.1	0.05	0.06		-				-
Pb_float	6	30								0.03					-
Zn condition	10	30	9.2	·			0.05				2.0	2.0			
Zn float	3	30	9.2												
							· 		<u></u>		· .				
Pb clean	3.5											+		<u>`</u>	
		<u> </u>		<u> </u>		<u> </u>		L							
PRODUCT	W				T	YSIS	% *	,	· · · · · · · · · · · · · · · · · · ·		D	ISTRI	BUTIC	N %	
	%	<u> </u>		Cu	Pb	Zn			-	<u> </u>		Cu	Pb	Zn	
C1 Pb conc.	24			3.44		17.14					*	2.0	81.9	13.5	
Cl Pb tail	28	•0		0.35	7.05	56.65			. •			9.6	11.9	51.4	
Ro Pb conc	52	.3	ŀ	1.79	29.63	38.30					9:	1.6	9 3.8	64.9	
Zn conc	20.	.4		0.29	3.26	49:00						5.8	4.0	32.4	
Ro tail	27.	.3		0.10	1.35	3.06						2.6	2.2	2.7	
Feed (calcd)	100.	.0	-	1.02	16.59	30.86	.~				100	0.0	.00.0	100.0	
Zn conc plus cl Pb tail	48.	.4		0.32	5.45	53.42					1.5	5.4	15.9	83.8	
						-									
REMARKS: * From Inte	rnal R	enort	MS-AC	-69-8	22										

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TEST NO. 29 SAN	1PLE: Ca	dillac	c Explo	oratio	on - Sul	phide	Ore							7,196	9
OBJECT OF TEST: Pre	eliminar	y Reag	gent In	nvesti	igation									.000-g	
						<u> </u>							ED B	Y: W.A.	W.
OPERATION	Time	%	pH	-	Jnit				······	igents,					
	min	Solids		L	used	NaCN	ZnS04	Ca0	A.31	Z-11	404	DF250	CuSO	4	<u> </u>
Grind (74.5%-200 m)	15	67		7 x	: 14 RM	0.2	0.8	1.0	0.04						
Condition	5	45	7.0	100	0-g cel	1				0.2	0.05				
Pb float	6	25	7.0							-		0.03			
Zn condition	10	30	10.1					2.0					2.0		
Zn float	6	30	10.1		, ,,					0.05					
Pb clean	2			50	0-g cel	1									
					, <u></u>										
					<u></u>										-
PRODUCT	w	T	·	•	ANAL	YSIS	% *	L	I		DI	STRIE	UTIO	N %	
	%	ó		Cu	Pb	Zn					Cu	1	РЪ	Zn	
C1 Pb conc C1 Pb tail	64 13			1.39 0.47	21.92 5.92							9.1	91.6 5.1	83.8 12.3	
Ro Pb conc (calcd)	77	.6		1.23	19.18	36.99					95	5.4	96.7	96.1	
Zn conc	5	•4		0.36	3.82	11.50					1	.9	1.4	2.1	
Ro tail	17	.0		0.16	1.74	3.24					2	.7	1.9	1.8	
Feed (calcd)	100	.0		1.00	15.38	29.88					100	.0 10	0.00	100.0	
REMARKS: * From Int	ernal H	Reports	MS-A	C-69-	940		···· ,· • ·· • • •								
REMARKS: * From Int	ternal I	leports	s MS-A	C-69-1	940						. <u></u>	<u></u>	<u></u>	<u>_</u>	

TEST NO. 30 SAM	PLE: Ca	dillac	Explo	oratic	on - Sul	phide	Ore					1		. 7, 19	69
OBJECT OF TEST: Grin	d coar	ser. R	eagent	ts sam	ie as Te	st 29	-							1000-g	
												J	STED E	3Y: W.A.	W.
OPERATIÓN	Time	%	pН	1	Jnit			; 	·	igents,					,
	min	Solids		، 	Jsed	NaCN	ZnSO ₄	CaO	A.31	<u>Z-11</u>	404	DF25	50 CuSC	4	
Grind (58%-200 m)	10	67		<u>7 x</u>	: 14 RM	0.2	0.8	1.0	0.04						
Condition	5	45	7.1	100	0-g cel	1				0.2	0.05				
Pb float	6	30			•							0.0)3		
Zn condition	10	_30	10.1					2.0			· · ·		2.0		
Zn float	3											0.0			
Pb clean	2		·	50	0-g cel	1						<u> </u>			_
					· · · · · · · · · · · · · · · · · · ·					·					
						<u> </u>						<u> </u>			
PRODUCT	W	11	· · · · · · · · · · · · · · · · · · ·	<u></u>	ANAL	YSIS	% *	·			DI	STR	IBUTIC	N %	
	%	6		Cu	Pb	Zn					(Cu	Pb	Zn	
C1 Pb conc	32	.3		2.3	38.24	31.24	•				72	4. 8	85.7	33.0	
Cl Pb tail	36	•4		0.5	3.61	47.82						3.3	9.1	57.0	
Rougher Pb conc	68	.7		1.35	19.89	40.00					93	.1	94.8	90.0	
Zn conc	6	.7	-	0.39	4.20	33.00					. 2	.6	2.0	7.2	
Rougher tail	24	.6		0.17	1.90	3.40					4	.3	3.2	2.8	
Feed (calcd)	100	.0		0.99	14.41	30.54					100	0.0	100.0	100.0	
Zn conc plus Cl Pb tail	L 43	1		0.48	3.70	45.52					20	.9	11.1	64.2	
• •														-	
REMARKS. * Enom Int				<u> </u>											

REMARKS: * From Internal Report MS-AC-69-940

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	APLE: Ca						re						. 7, 19	
OBJECT OF TEST: Re	peat of	Test 2	28 but	at c	oarser	grind							1000-g	
													SY: W.A.	W .
OPERATION	Time	%	pН	3	Jnit	Ammo	r		·····	·	b per tor	· · · · · · · · · · · · · · · · · · ·		
	min	Solids		L	Ised	Phos	Z - 11	404	A.31	DF250				-
Grind (58%-200 m)	10	67		<u>7 x</u>	14 RM	4.0								
Condition	5	45	7.9	100	0-g cel	1	0.10	0.05	0.04					1
Pb float	2.5	30	7.9											
Seavenger float	4.5	30	7.9					<u> </u>						
														<u>†</u>
PRODUCT	W	11				_YSIS	%*	1					·	. <u></u>
	%	o		Cu	РЪ	Zn					Cu	Pb	Zn	
Pb conc	24	•1		3.70	58.20	16.05					86.7	87.5	12.2	1
Scavenger conc	26	.5		0.33	4.36	57.70					8.6	7.2	48.2	1
Rougher tail**	49	•4		0.10	1.71	25.45					4.7	5.3	39.6	
Feed (calcd)	100	.0		1.03	16.03	31.73					100.0	100.0	100.0	
	a de la constante de la constante de la constante de la constante de la constante de la constante de la constan	a na si na si na si na si na si na si na si na si na si na si na si na si na si na si na si na si na si na si n												
REMARKS: * From In	iternal	Report	MS-AC	C-70-8	3	I			1			<u> </u>	<u>L</u>	
** No zinc flotation	attempt	ed.												

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TEST NO. 32 SAM	PLE:Cad	lillac	Explor	ation	n - Sulp	hide O	re	· · · · · · · · · · · · · · · · · · ·				DATI	E: Nov	7.10,1	969
OBJECT OF TEST: Rep								Eloat a	as in 7	Cest 31	-			1000-g	
												·····	EDE	3Y: W.A.	W
OPERATION	Time	%	рН		Jnit			1	···	gents,	· · · · · · · · · · · · · · · · · · ·		.		
	min	Solids	\$		Jsed	NaCN	ZnSO4	<u>Ca0</u>	A.31	<u>z-11</u>	404	DF250	CuSC	94	
Grind (58%-200 m)	10	67		73	<u>(14 RM</u>	0.2	0.8	1.0	0.04						
Condition	5	47	7.1	100)0-g_cel	1				0.1	0.05				
Pb float	4	30	. 7.1												
Scavenger float	4	30	7.1		45		· · · · ·					0.015			·
Zn condition	10	30	10.4		· · · · · · · · · · · · · · · · · · ·			2.0			· · ·		2.0)	
Zn float	2														
PRODUCT	W	T	i		·	YSIS	% *					STRIE			1
	=			Cu	Pb	Zn						Cu	<u>Pb</u>	Zn	
Pb conc	52	.6		1.61	25.00	36.00					. 85	5.9	88.3	64.5	-
Scavenger conc	29	.8	× .	0.33	4.45	32.00	· · ·				ç	9.9	8.8	32.5	
Zn conc	1	.6		0.35	4.00	10.84						.6	0.5	0.6	
Rougher tail	16	.0		0.22	2.22	4.44					3	.6	2.4	2.4	
Feed (calcd)	100	.0		0.99	14.90	29.36					100	0.0 1	00.0	100.0	
Scav. conc + Zn conc	31	.4		0.33	4.43	30.92					10	.5	9.3	33.1	
REMARKS: * From Int	ernal l	Report	MS-AC	-70-8	3									· · ·	
			1 4				· · ·								
														· · · · · · · · · · · · · · · · · · ·	

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TEST NO. 33 SAMP	LE: C	adilla	ac Expl	orati	on - Su	lphide	Ore					DAT	E: Nov	. 10, 1	969
OBJECT OF TEST: Repe	at of	Test 3	32 at f	iner	grind										
													TED B	Y: W.A.	W
OPERATION	Time	%	рН	1					,	<u> </u>		1			· · · · · ·
	min	Solids	8	u	sed	NaCN	ZnS04	Ca0	A.31	Z-11	404	DF250) <u>CuSO</u>	4	
Grind (91.5%-200 m)	20	67		7 x	14 RM	0.2	0.8	1.0	0.04			<u> </u>			
Que ditting		1.7	7 1	100	0 1	1				0.2	0.05				
Condición		4/	/•1	100	U-g Cel	4				0.2	0.05	1			
Pb float	2	30			· · · · ·							1			-
Scavenger float	4	30		<u> </u>	i				_			0.015	5		
CHARGE: 10 CHARGE: 10 Time $\medskip min Solids \medskip min Solid \medskip min Solids \medskip min Solids \medskip min Solids \medskip min Solids \medskip min Solids \medskip min Solid \medskip m$															
	1	25	10.4					2.0		0.05		<u> </u>			
						-	1			0.05				1	
RRODUCT					ANAI	YSIS	% (1)				DI	STRI	BUTIO	N %	
	9	6		Cu	Pb	Zn			_			Cu	Pb	Zn	
Pb conc	27	.0		2.69	49.20	16.97					7.	5.9	84.0	15.3	
Scavenger conc	47	.0		0.42	4.00	50.00					2	0.6	11.9	78.5	
Ro tail	26	.0		0.13	2.48	7.20						3.5	4.1	6.2	
Feed (calcd)	100	.0		0.96	15.81	29.95					10	0.0	100.0	100.0	
DEMADICO N. No. stars f		<u> </u>	<u> </u>									<u> </u>		1	
(1) From Internal Re	port M	S-AC-7	-83 70-83												
						<u> </u>									

TEST NO. 34 SAMP					on - Sul			1	- 61	. 4.	· · · · · ·			• 4, 196 1000-g	9
OBULCI ON TEST. Repe	acor	lest	JI WI		inger con	101,2101	ing and	i a zir	nc rioa	IC				3Y: W.A.	W.
OPERATION	Time	%	- 11		Jnit	Ammo			Rea	gents,	lb per				
OPERATION		Solids	рН		used	Phos	Z-11	404	A.31	Ca0	CuSO/	Z-200)		1
Grind (58%-200 m)	10	67		7 x	14 RM				· · · ·						
Condition	25	45	7.1	100)-g cell	4.0	0.05	0.05	0.02		l				
Pb float	3	25	7.1						0.02						
\ \	-							· · ·							
Zn condition Zn float	<u>10</u> 3	25 25	9.0							2.0	2.0	0.05	_		
Pb conc clean	11/2			250)-g cell										
Zn conc clean	3)-g cell		· .								
	w	 		1			0/ -5				<u> </u>	STRIE			
PRODUCT	%			Cu	Pb	Zn	<u>%</u>		-				Pb	Zn	
Cl Pb conc Cl Pb tail	24				54.75			· .			81		81.3 6.4	14.7 39.1	
Ro Pb conc	45.	.6		1.98	31.75	35.56					86	5.6	87.7	53.8	
Cl Zn conc Cl Zn tail	24.		1	0.32 0.64	4.36 9.38	51.07 14.00						.6	6.6 3.5	42.2 2.8	
Ro Zn conc	31.	1		0,39	5.36	43.68					11	.•4	10.1	45.0	
Rougher tail	23.	3		0.09	1.55	1,50			-		2	.0	2.2	1.2	
Feed (calcd)	100.	0		1.04	16.50	30.15		×			100	.0 10	0.00	100.0	
Cl Pb tail + Cl Zn conc	46.	0		0.30	4.67	53.24					13	.1	13.0	81.3	
REMARKS: * From Inte	ernal	Report	MS-A	C-70-9	93									•	
					· ··				•						

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					on - Sul			<u> </u>				DAT	E: De	c. 4, 19	969
DBJECT OF TEST: Rep	eat of	Test 3	1 wit	h zino	c float	instea	d of s	cavenge	er floa	t				L000-g	
													TED E	3Y: W.1	A,W
OPERATION	Time	%	рН		Jnit	Ammo	·	·,			lb per	ton			
	min	Solids		ر ا	ised	Phos	Z-11	_404	A.31	<u>Ca0</u>	CuS04	DF25	0		
Grind (58.0%-200 m)	10	67		<u>7 x</u>	14 RM	4.0							_		
Condition	5	45	.8.2	1000)-g cell		0.1	0.05	0.04						
Pb float	5	25	8.2		· · · · · · · · · · · · · · · · · · ·										
Zn condition	5	25	8.2							2	2				
Zn float	10	25	8.2									0.03			
													1		
PRODUCT	W	11		Cu	Pb	_YSIS Zn	% *	1	1			STRIE Cu	Pb	N % Zn	
Pb conc	22	3		3.60	61.95			<u>.</u>			70	9.1	85.1	6.7	
Zn conc	48			0.36	3.83										
													11.3		
Ro tail	29			0.13	2.00						3	.8	3.6	8.1	
Feed (calcd)	100	•0		1.01	16,24	30.41					100	0.0 1	00.0	100.0	
								-							
·															
EMARKS: * From In	ternal	Report	MS-A	C-70-	83										

TEST NO. 37 SAM	PLE: Ca	dilla	c Expl	orati	on - Sul	.phide	Ore		·					30, 19	69
OBJECT OF TEST: Repe	eat of	Test 3	33 wit	h zino	c float	instea	d of so	avenge	er floa	ıt				1000 - g	
												· · · · ·	FED B	Y: W.A.	W.
OPERATION	Time	%	Ha		Jnit					igents,	• • • • • • • • • • • • • • • • • • •				
	min	Solide	5		used .	NaCN	ZnS04	Ca0		<u>z-11</u>	404	DF250	CuSO	4	
Grind (91.5%-200 m)	20	67		7 x	14 RM	0.2	0.8	1.0	0.04						
	ļ			-								<u> .</u>			
Condition	5	45	7.1	1000)-g cell		·			0.1	0.05	<u> </u>			·
	2	30	7.1		· · ·										
Pb float	2	- 50	/•1												
Zn condition	5	30	9.6	+	<u></u>			1.0		0.1		0.015	1.0		
	<u>ÿ</u>				·····							1.		•	
Zn float	7	30	9.6								0.05				
		<u> </u>													<u> </u>
·		· ·			•		ļ		 			<u> </u>			
, 				1			<u> </u>	[<u> </u>	<u> </u>			<u></u>	
PRODUCT	. W	1		Cu	ANA Pb	_YSIS Zn	%* .	1				STRIE Cu	<u>Pb</u>	N %	
				υų	FD								E D	211	
Lead concentrate	25	.8		2.88	52.40	17.20	-				7	5.4	82.0	1,4.4	
Zinc concentrate	50	•3		0.42	4.51	49.92	* . •	• • •			2	1.4	13.8	81.7	
Tailing	_23	•9		0.13	2.91	5 <u>°</u> 00						3.2	4.2	3.9	
Feed (calcd)	100	.0	(0.98	16.48	30.74					1.0	0.0 1	00.0	100.0	•
				,			· .								
· · ·					·				-						
REMARKS: * From Int	ernal	Report	MS-A	2-70-9	98		•		· · ·						• • •
					· •						. •				
				<u>`</u>											

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					n - Sulp				<u> </u>			DATE	E: Dec	<u>. 30, 1</u>	969
DBJECT OF TEST: Aff	ect of	sodium	sul _f	ohite a	as zinc	depres	sant					· · · · · · · · · · · · · · · · · · ·	RGE: 1	Y: W.A.	1.7
	1	1			•	1			Rea	aente	lb per			1. W.A.	w .
OPERATION	Time min	% Solids	рН	1	Jnit used	NaCN	ZnS04	Ca0	Na ₂ SO ₃				DF250	0 CuSO4]
Grind (91.5%-200 m)	20	67		7 x	14 RM	0.2	0.8	1.0	1.0	0.04				-	
Condition	5	50		1,000)-g cell						0.10	0.05			
Lead float	3	25	7.2												
Scavenger float	2.5	25	7.2										0.01	5	+
Zinc condition	5		10.3					1.0			0.10		0.01	5 1.0	
Zinc float	3	25	10.3												
Lead clean	3			250)-g cell							<u></u>			
PRODUCT	W 9	11			TT	LYSIS	% *	·····				STRIB	ī		
				Cu	РЪ	Zn						<u>hu </u>	РЪ	Zn	
Cl Pb conc Cl Pb tail	30 26			2.61 0.27	44.38 3.16							6 2	85.1 5.1	25.6 45.2	
Ro Pb conc (calcd)	56	.9		1.54	25.47	37.33					89	.8	90.2	70.8	
Scavenger conc	18	•2		0.26	4.16	35.32					4	••8	4.7	21.4	
Zinc conc	7	•4		0.27	4.16	15.51					2	.1	1.9	3.8	
Rougher tail	17	•5		0.18	2.91	6.78					3	.3	3.2	4.0	
Feed (calcd)	100	.0		0.97	16.07	30.00					100			100.0	
Combined Zn conc**	51	.7		0.26	3.65	40.86					14	•1 1	1.7	70.4	
REMARKS: * From In ** Combination of Cl	ternal] Pb tail	Report , scav	MS-A enger	C-70-9 conc	9 and zin	c conc.	<u>, </u>	<u>I</u>				<u>1, , , </u>			

					on - Sul			_,					E: Dec.		.969
OBJECT OF TEST: Repe	at of	Test	38 at	a coa	arser gr	ind							RGE: 1	-	Tal
						1			Bee		lb per		TED BY		
OPERATION	Time min	% Solids	pH	1	Jnit used	NaCN	ZnS04	Na ₂ S03		A.31		404	DF250	CuS04	
Grind (74.5%-200 m)	15	67		7 x	14 RM	0.2	0.8	1.0	1.0	0.04					
Condition	5	50.	8.0	100	D-g cell						0.05	0.05		· ·	
Lead float	6	30	8.0												
Scavenger float	4	30	7.4		······································						0.05	 	0.015		
Zinc float	5	30	9.7					-	0.5		0.05			0.5	
Clean lead zonc	3			250)-g cell										
	w	1		<u>.</u>	ANAL	I YSIS	% *				· DI	STRI	BUTION	%	
	%			Cu	РЪ	Zn					<u>F</u>	рЪ	Zn		
Clean Pb conc Clean Pb tail Rougher Pb conc (calcd)	23 20 44	.2		0.43	54.60 4.17 31.45	1	、 、、 、 、 、		· · ·		5	•.9 •.5 •.4	12.9 4.9 17.8		
Scavenger conc Zinc conc	40. 3.	61		0.12	2.18 10.55							.8 .2	76.3 3.2		
Rougher tail	12.	0		0.10	2.06	6.47	y T				1	.6	2.7		1949 - 19
Feed (calcd)	100.	ο			15.31	28.90					100	•0 •]	L00.0		
Scav. conc plus Zn conc	44.	0		:	2.79	52.26	· . ·				8	•0	79.5	· .	
							•								
REMARKS: * From Intern	11 Ro	li nort M	<u> </u>	70_00	and Por		E		<u> </u>	<u>_H</u>	11 70	<u> </u>	<u> </u>	· 1	

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TEST NO. 40 SAMP	LE: Ca	dillac	Explo	ration - Sul	phide	Ore						E: Jan.		'0
OBJECT OF TEST: Sul	phidiz	e lead	miner	als					,			RGE: 10		
									<u> </u>		·	FED BY	. W.A.W	1.
OPERATION	Time	%	рН	Unit			1		.gents,	r	T		1	···
		Solids		used		ZnSO4	CaÒ	A.31	<u>Z-11</u>	404	Na ₂ S	DF250	CuSO4	
Grind (74.5%-200 m)	15	67		7 x 14 RM	0.2	0.8	1.0	0.04			ļ			
		50		1000 11			<u> </u>		0.05	0.05				
Condition	5	50		<u>1000-g cell</u>					0.05	0.05				
Lead float	5	30	8.2						0.05		2.0	0.015		
					1							100020		
Zinc condition	5	25	11.1				2.0						1.0	
			11 0											
Zinc float	7	25	11.0						0.05		<u> </u>	0.03		
Clean lead conc	2			250-g cell							<u> </u>			
- orean read cone				230-g Cell	1									
PRODUCT	W	т		ANAL	YSIS	% *				DI	STRIE	UTION	%	
FRODUCT	%	6		РЪ	Zn		[P	'b	Zn		
					16 00							10 7		
Clean Pb conc Clean Pb tail	25			53.80 10.89	16.20 42.36						5.3 2.7	5.5		
clean PD tall		• •		10.07	42.50									
Rougher Pb conc (calcd)	29.	.2		48.07	19.70					8	8.0	19.2		
Zinc conc	46.	2		3.05	50.10						8.8	77.6		
Zine cone	40.	·		5.05	J 0.10									
Rougher tail	24.	.5		2.09	3.89						3.2	3.2		
$T = 1 \left(-1 - 1 \right)$	100.			15.90	29.90					10	0.0 10	0.0		
Feed (calcd)	100.	.0		15.90	27.70						ł			
Cl Pb tail + Zn conc (calcd)	50.	.2		3.66	49.50					1	1.5	83.1		
•														
REMARKS: * From Inter	nal Re	eport N	íS-AC-	70-99 and Bor	ndar-Cl	egg Co	. Ltd.	, Repo	rt A-1	1-70.				
	<u></u>									•				

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				oration - Sul	phide	Ore			· · ·				. 12,	1970
DBJECT OF TEST: Flo	otation	n at 15	% soli	lds							<u> </u>	RGE: 1		• • •
			· · · · · ·		;			Rea	igents,	lh per		IED B	Y: W.A	. W .
OPERATION	Time min	% Solids	рН	Unit used	NaCN	ZnS04	Ca0	A.31			· · · · · ·	CuSO	4	
Grind (91.5%-200 m)	20	67		7 x 14 RM	0.2	0.8	1.0	0.04						
Condition	5	50	7.2	2000-g cell					0.1	0.05	0.01	5		
Lead float	5	15	7.2											
Zinc condition	5	15	9.0			·	1.0		0.2	0.10	0.03	1.0		_
Zinc float	5	15	9.0				 						<u>`</u>	_
Clean lead conc (twice)	2		· · · · · · · · · · · · · · · · · · ·	500-g cell		2				 				
		<u>г. </u> т.		ANAL	L YSIS	% *	Į	ļ		D	STRIE	BUTIO	N %	
PRODUCT	9	6 . 		Pb	Zn						Pb	Zn	,	
Clean Pb conc Clean Pb tail	21 45			56.95 7.00	18.28 51.42					(3.3 9.4	12.5 75.7		
Rougher Pb conc (calcd)	66.	.9		22.83	40.92					9	2.7	88.2		
Zinc conc	15.	2		5.71	20.39						5.3	10.0		
Rougher tail	17.	9		1.89	3.20						2.0	1.8		
Feed (calcd)	100.	.0		16.48	31.04					10	0.0	100.0		
Combined Cl Pb tail and In conc (calcd)	60.	9		6.68	43.67					2	4.7	85.7		

TEST NO. 42 SAMP	LE: Ca	dillac	Explo	ratio	n - Sul	phide	Ore								. 13, 1	.970
OBJECT OF TEST: Flota	ation	at 33%	solic	ls			<u> </u>						CHAF	RGE:	1000-g	
														ED B	Y: W.A.	.W.
OPERATION	Time	%	На	U	nit							lb per				
OFERATION	min	Solids		u	sed	NaCN	ZnS04	Ca0	A. 31	Z-	11	404	DF250	CuSO	4	
Grind (91.5%-200 m)	20	67		7 x	14 RM	0.2	0.8	1.0	0.02							
Condition	5	50	7.2	1000	-g cell					0.	05	0.10				
	,					+	+			-				1		
Lead float	6	33	7.2													
Zinc condition	10	30	9.4					1.0		0.	20	0.10	0.03	1.0	 	
Zinc float	6	30					-		<u> </u>							
Clean Pb conc	2	8		500	-g cell									<u> </u>		
1		1 	l	1		1			<u> </u>	1			STRIB			1
PRODUCT	W .			. (1)		YSIS	· · · · · · · · · · · · · · · · · · ·					·				
		·		$Ag^{(1)}$	Cu	<u>Pb</u>	Zn			_#			lg	<u>Pb</u>	Zn	
Cl Pb conc Cl Pb tail	20 10			5.94 3.16		67.80 8.28	1						7.0 +.6	83.6 5.2	4.0 16.2	
Rougher Pb conc (calcd)	30	• 5	2	7.91		47.37	19.67					91	6	88.8	20.2	
Zinc conc	49	•2		3.08		2.61	46.30					5	5.7	7.8	76.9	
Rougher tail	20	.3		1.23	0.13	2.76	4.24					2	.7	3.4	2.9	
Feed (calcd)	100	.0		9.30		16.39	29.64					100	.0 1	0.00	100.0	
Combined Cl Pb tail and Zn conc (calcd)	1 59	•5		3.17		3.59	46.36					20	.3	13.0	93.1	
REMARKS: * From Inter		-	4S-AC-	70 - 88	and 99	and B	ondar-C	legg	Co. Lto	 1. Re	poi	rt A-1	1-70			
(1)ounces p	er tor	n				<u></u>										

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TEST NO. 43 SAMP	LE: Ca	dillac	Exp	lorati	on - Su	lphide	Ore					DATE		. 15,	1970
OBJECT OF TEST: Copp	er-lea	id sepa	ratio	on.								h		3000-g	
												4	ED B	Y: W.A.	J
OPERATION	Time	%	На		Unit				Rea	igents,	lb per	ton	····		
	min	Solids	P		used	NaCN	ZnSO4	CaO	A.31	<u>z-11</u>	404	DF250	CuSO	4 S.B.	H ₂ SO
Grind (74.5%-200 m)	15	67			14 RM		1.0	1.0	0.02			·	<u> </u>		
Condition	5	50	6.9	200	0-g cell	L]			·	0.05				_	_
Lead-copper float	10	32	6.9			· · ·				0.017	+0.017	+ 0.03	ļ		
Zinc condition	10		9.8				<u> </u>	1.0		0.20	0.10		2.0	- · ·	
Zinc float	8	30					<u> </u>			<u> </u>		0.03			
Clean zinc conc	2				<u>0-g cell</u>					· · · · · ·	<u> </u>	ļ	<u> </u>		
Clean Pb-Cu conc	3	10		100	0-g cell	0.1	0.15								_
Reclean Pb-Cu conc	3			100	0-g cell	0.05	0.15					<u> </u>			
Re-Reclean Pb-Cu conc	5			_100	0-g cell		1.0								
Lead-copper separation	3		5.5	100	0- <u>g_cel</u> 1									1.5	10
Clean Cu conc	2			50	0-g cell									2.0	
Reclean Cu conc	2			50	0-g cell								· ·	2.0	
	W	τ			ANA	LYSIS	%(1)				DI	STRIB	UTIO	N %	
PRODUCT	. %	6		Ag (2)(5) Cu	Pb	Zn		1.			Ag C	u ⁽⁴⁾	Рb	Zn
Reclean Copper conc	2.	0		220.46	27.90	8.30	12.20				4	4.8	55.9	1.1	0.8
Lead conc. (3)	14.			21.04		72.90	6.10						18.4	68.6	3.0
Re-Reclean Pb-Cu conc (calcd) 16.	7		44.92	4.44	65.16	6.83				7	6.3	74.2	69.7	3.8
Pb-Cu clean & reclean tai	1 11.	9		6.29	. х.	12.50	50.90					7.6		9.5	20.5
Pb-Cu Re-reclean tail	4.	- 11		15.86	1 1	47.80	20.00					7.3		13.8	3.0
Pb-Cu rougher conc (cale	cd)33.	1		27.00		43.87	24.47				9	1.2		93.0	27.3
C1 Zinc conc	32.	0		1.50		0.85	60.90			- I		4.9		1.7	65.8
Cl Zinc tail	8.	*1		3.34	1	5.60	20.60					2.9		3.0	-5.9
Ro Zinc conc (calcd)	40.	4		1.88		1.84	52.52					7.8		4.7	71.7
Rougher tail	26.	5		0.385		1.35	1.08		÷ .			1.0		2.3	1.0
Feed (calcd)	100.	0		9.83		15.62	2 9. 60	•			100	0.0		100.0	100.0
REMARKS: * Stage adde	ed	(1 (3) Lea	dar an d cond tails	nd Clegg plus c	Report lean &	t No. A reclea	14-9. n	(4) I	Based o	nternal on Assa per to	av Head	t MS	-AC-70- 0% copp	124• per.

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			c - Ex	cplora	tion - S	ulphid	e Ore							27, 19	70
OBJECT OF TEST: Pro	moter	Z-200												3000-g	
		1								· · · · · · ·			TED B	Y: W.A.	W.
OPERATION	Time	1	рH	1	Jnit		T	·		gents,					
	min	Solids	•	L	used	ZnS04	Ca0	A.31	Z-200	DF250	<u>z-6</u>	CuS04	NaCl	N	
Grind (74.5%-200 m)	15	67		<u>7 x</u>	14 RM	1.0	1.0	0.02				<u> </u>			
Condition	5	50	6.9	200	0-g cel:				0.03	0.015					
Pb float	10	35	6.9						0.10						
Pb float	6	35	5.8		·				0.10		0.03				
Zn condition	10	35	10.0				1.0			0.03		1.0	- <u> </u>		
Zn float	6	35	10.0								0.10				
Pb clean	2			100	0-g cell	0.2							0.1	 L	
Zn clean	2	<u> </u>	<u> </u>	200	0-g cell										<u> </u>
PRODUCT	W.	13		4-(1)		YSIS Zn	% * .	1						·	
				Ag(1)								g	Pb	Zn	
Clean Pb conc Clean Pb tail	14	11		47.76 13.12		13.45 33.80					1	.9 . 2	42.2 20.4		
Rougher Pb conc (calcd)	28	.7		30.14	38.85	23.80					8	86.9	62.6	22.7	
Clean Zn conc Clean Zn tail	24			2 .1 8 2 . 22	6.87 14.30							5.4	9.5 19.2		
Rougher Zn conc (calcd)				2.20	10.52						1	.0.7	28.7		
						2.93						2.4	8.7		
Rougher tail	22.			1.04	6.79										
Feed (calcd)	100.	.0		9.96	17.81	30.16					10	0.0	100.0	100.0	
REMARKS: *From Inte			MS-AC	C-70-1	24 and 1	Bondar-	Clegg	Co. Lt	d., Rep	port A	-20-70				
(1) Ounces	per 1	lon.									_				

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				orati	on Sampl	e No.	2, Lots	32 , 3	3 and	34				ril 14,	1970
OBJECT OF TEST: Pb -	Zn se	parati	.on										ARGE:		
					····					<u> </u>			STEDE	BY: W.A	.W.
OPERATION	Time	% Salisia	рН	1	Jnit Jsed	Ammo	1 101]		gents,	· · · ·			10007	
		Solids				Phos.	404	<u>Z-11</u>	A. 31	Na ₂ S	Na ₂	<u>U3Na2</u>	<u>toyCuSC</u>	14 3037	DF250
Grind (53.7%-200 m)	15	67			14 RM	4.0	<u> </u>						·		
Condition	5	45	7.0	1000	-g cell		0.40								
No. 1 Pb floation	3	30									•				
No. 2 Pb floation	9	25	8.3				0.20	0.10	0.04	4.0					
Zn condition	10	25				4.0					6.0	6	0 1.	0	
Zn floation	12	25	10.3		······					15.0				0.60	0.03
No. 1 Pb conc clean	1			250	-g cell										
No. 2 Pb conc clean	2			500	-g cell										
										•					-
Zn conc clean	3			500	-g ⁻ cell	· ·						·			
PRODUCT	w-	11			ANAL	YSIS	% *				Ε	DISTR	IBUTIC	DN %	
	%	·		РЪ	NS Pb	S.Pb	Zn	NS Zn	S. Zi	n Pb	1	NS Pb	S. Pb	Zn	NS Zn
No. 1 Clean Pb conc	4.			1.12	36.12	25.00		5.58	0.4	13	. 1	8.2	1	1.5	1.5
No. 1 Clean Pb tail	5.	17		6.32	33.43	2.89		14.41		11	.6	8.7		4.3	4.3
No. 1 Ro Pb conc (calcd)	10.	1	4	7.86	34.68	13.18	10.59	10.59	0.2	21	•2	16.9	61.2	5.8	5.8
No. 2 Clean Pb conc	9.	4	3	2.37	30.37	2.39	16.00	15.79	0.2	13	.5	13.8	10.3	8.2	8.2
No. 2 Clean Pb tail	13.			4.58	23.61	0.97		18.07	0.3	18 .		15.3	6.0	13.5	13.4
No. 2 Ro Pb conc (calcd)	11	11		7.95	26.40	1.55		17.13	0.28			29.1	16.3	21.7	21.6
Combine Ro Pb conc	32.	9	3	4.06	28.94	5.12	15.32	15.03	0.29	49	•1	46.0	77.5.	27.5	27.4
Clean Zn conc	10.	8	3	9.57	38.12	1.45	16.80	16.72	0.08	3 18	.7	19.9	7.2	9.9	10.0
Clean Zn tail	9.	11		3.62	22.43	1.19	19.20		0.14	11	1	10.3	5.2	10.0	10.0
Ro Zn conc (calcd)	20.	3	3	2.11	30.78	1.33	17.92	17.82	0.08	3 28	.5	30.2	12.4	19.9	20.0
Rougher tail	46.	11		0.97	10.50	0.47		20.33	0.27	11		23.8	10.1	52.6	52.6
Feed (calcd)	100.	0	2	2.86	20.68	2.18	18.32	18.08	0.24	+ 100	.0 1	00.0	100.0	100.0	100.0

REMARKS: * From Internal Report MS-AC-70-431

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	MPLE: Cad			oratio	n Sample	No. 2	, Lots	32, 3	3 and 3	34			E:Apri		970
OBJECT OF TEST:	Pb - Zn s	separat	tion										RGE: 1		Ţ.Ţ
				· · · · · · · · · · · · · · · · · · ·							11		TED B	Y: W.A.	W
OPERATION	Time	%	рH	1	Jnit	Ammo	4.04	7 11		igents,					
	min	Solids	il		used	Phos	404	2-11	A. 51	DF250	Na ₂ S	Na ₂ C	D3 Nazsi	CuSO4	<u> </u>
Grind (53.7%-200 m)	15	67	-	7 x	14 RM	4.0								-	
Condition	5	45	6.8	100	D-g cell		0.40								
No. 1 Pb floation	5	30						0.10	0.04	0.03		 			
No. 2 Pb floation	8	30	9.3				0.20				4.0				
Zn condition	10	25	10.4									6.0) 8.0	1.0	
Zn flotation	4	25	10.4				0.20	0.10		0.03	15.0				
<u>,</u>		<u> </u> 	1	1	ANAL	I YSIS	%*		l	l	L DI	STR	BUTIO	<u> </u>	L
PRODUCT	11	6		РЪ	Zn							Pb	Zn		
No. 1 Pb conc	59.	.7	-	30.31	17.41						8	3.2	58.2		
No. 2 Pb conc	6.	.0		25.00	17.41							6.9	5.9		
Pb conc (calcd)	65.	.7		29.82	17.41						9	0.1	64.1		
Zn conc	6.	.2		16.64	17.58							4.7	6.1		
Rougher tail	28.	.1		4.00	18.96							5.2	29.8		
Feed (calcd)	100.	.0		2 1.7 5	17.86						10	0.0	L00.0		
				10.70	510										
REMARKS: * From]	urer na i	vebori	L HO-A	10-/0-											

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MINES BRANCH FLOTATION TEST REPORT DATE: April 16, 1970 TEST NO. 47 SAMPLE: Cadillac Exploration Sample No. 2, Lots 32, 33 and 34 CHARGE: 1000-g OBJECT OF TEST: Pb-Zn selective flotation TESTED BY: W.A.W. Reagents, Ib per ton Time % Unit OPERATION pН min Solids used Na₂CO Na₂SiO₂ Na₂S 404 Z-6 CA A.31 P.0. 3037 Grind (53.7%-200 m) 15 67 7 x 14 RM 1000-g cell 0.10 0.04 Condition 5 50 3.5 6.5 No. 1 Pb flotation 30

0.10

0.10

0.1

.

2.0

2.0

1.0

3.0 1.0 10.0 0.20

1.0

0.20

0.20

0.10

0.03 0.40 0.03

43

Condition

Condition

No. 2 Pb flotation

No. 3 Pb flotation

Condition

Zn flotation

5

5

3

5

3

[.] 3

30

30

30

30

30

25

7.5

10.5

														1
]
PRODUCT	WT			ANAL	YSIS	% *				DI	STRIE	BUTION	1 %	
	%		РЪ	ZN					·	P	Ь	ZN		
No. 1 Pb conc	7.7	5	0.00	9.76						1	7.7	4.0		
No. 2 Pb conc	24.7	1 1		13.00			}				1	7.2		
No. 3 Pb conc	14.2		1	18.30					1		1	3.9		
NO. 3 PD CONC	14.2		0.00	10.50						1	10.5			
Total Pb conc (calcd)	46.6	4	4.58	14.08						9	5.2 3	35.1		
									1					
Zn conc	32.8		2.15	25.59							3.2 4	4.8		
Bulk conc (calcd)	79.4	2	7.05	18.84	1					98	3.4 7	79.9		
					.									
Rougher tail	20.6		1.66	18.26						.]	1.6 2	20.1		
Feed (calcd)	100.0	2	1.82 []	18.72						100	0.0 10	0.0		
													•	
	<u></u>							<u>, </u>		I	<u> </u>	<u></u>		
REMARKS: * From Inte	ernal Repo	ort MS-A	C-70-50	07.										

	MPLE: Ca			oratio	on Sample	No. 2	, Lots	s 32 , 3	3 and	34			E: April		
OBJECT OF TEST: 1	ead-zinc	separa	ation										TED BY		
OPERATION	Time	%	рН	1	Jnit				Rea	igents	, lb per				
OPERATION	min	Solids	рп		used	Z-6	CA	Na ₂ CO:	Na2 <u>SiO</u> .	Na ₂ S	ZnS04	NaC	N 3037	404	
Grind (53.7%-200 m)	15	67		7 >	: 14 RM					1 i					
Condition	5	50		100	0-g cell	0.10	0.03								
No. 1 Pb float	3	30	6.5												
Condition	5		7.5					2.0	0.5	0.5	1.0	0.2	2		
No. 2 Pb float	3		8.8			0.10			0.5	0.5	<u></u>			0.2	
Condition No. 3 Pb float	3		9.3			0.10		+	0.5	0.5				0.2	
Zn condition	5		10.4			0,10			0.5	5.0			0.60	0.2	
Zn float	5				-								· ·		
PRODUCT	W	I			ANAL	YSIS	% *				DI	STRI	BUTION	%	
	9	6		Pb	ZN							РЪ	ZN		
No. 1 Pb conc	11.	14			10.73							3.5	6.3		
No. 2 Pb conc No. 3 Pb conc	27	.6 .2	1	2.37 2.22	11.69 21.15							6.4 5.3	17.2 5.9		
Bulk Pb conc (calcd)	43	.8	4	.7.33	12.59						9	5.2	29.4		
Zinc conc	30.	.3		2.31	32.25							3.2	52.3		
Bulk conc (calcd)	74	.1	2	.8 .9 2	20.62						9	8.4	81.7		
Rougher tail	25	.9		1.35	13.22							1.6	18.3		
Feed (calcd)	100.	.0	2	1.78	18.70						10	0.0	.00.0		
									<u> </u>	1					
REMARKS: * From	Internal	Report	: MS-A	.C-70-	518.										

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TEST NO. 51 SAMP	PLE: Ca	adillad	c Expl	oratio	on Sampl	e No.	2, Lot	s 32, 3	3 and	34		DATI	E: Apri	1 24,	1970
OBJECT OF TEST: Coar	se gri	ind											RGE: 20		
									·			TEST	ED BY	': W.A.	W.
OPERATION	Time	%	pH.		Init				Rea	gents	, lb per	ton			
	min	Solids		, u	ised	NaCN	ZnS04	Na ₂ CO ₃	Z-8	444	DF250	Na ₂ S	CuS04	3037	
Grind (approx. 35%-200	15	67	1	7 x	14 RM	0.50	1.50	3.0						1	
m)															1.
Condition	3	25	7.2	2000	-g cell				0.05						
			-		```										
No. 1 float	5	· · · · ·	9.0						0.05	0.25	0.04				
	·													· ·	<u> </u>
No. 2 "	- 5		·			ļ			0.10	0.50	0.05	<u> </u>			<u> </u>
~ ~ ~	<u> </u>				,			<u> </u>		0 7 -		· ·		- <u> </u>	<u> </u>
No. 3 11	5.						· · · · ·		0.10	0.50	0.05				·
		 	· · ·				· ·				<u> </u>				
No. 4 "	10				·	<u> </u>						2.0	1.0	1.2	
No. 5 "	5	<u> </u>	9.8	1		I			0.40	1.00			<u> </u>	0.6	<u> </u>
PRODUCT	• W	1	······	·		YSIS	% *		· · · · · · · · · ·		······		UTION	1. %	
	_	•		РЪ	ZN				· · · · · · · · · · · · · · · · · · ·	_		Pb	ZN		
No. 1 conc	6.	1	5	2.31	13.33						. 1	4.1	4.3	- [
No. 2 conc	5.				14.67							8.8	4.1		
No. 3 conc	14.				14.22								1.1		
No. 4 conc	34.				17.31								1.6		
No. 5 conc	13.	.4	1	4.99	19.56							8.9 1	3.8		
Rougher tail	25.	0	1	5.51	25.63						4				• `
Kougher call	2.5	2.	<u>ل</u> د.	J.JT	23.03						L	7.7 3	5.1		•
Feed (calcd)	100.	0	2	2.65	18.93	· ·					10	0.0 10	0.0		
			-												
. ·															
	-				ł					· ·					
											l		·].	·	
					<u> </u>			L	<u> </u>		<u> </u>		<u> </u>	<u> </u>	
REMARKS: * From Inte	rnal R	eport	MS-AC-	-70-53	1.					4	•	. · · · ·	s,		
					*		•		•	• .					
	··			<u></u>			·								

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······································	LE: Ca	adillac	Explo	oration	ı Sampl	e No.	2, Lot	s 32,	33 and	34		1	E: May		70
OBJECT OF TEST: Zin	c Reco	overy											RGE: 1		
		T										·	TED BY	. W.A.	N .
OPERATION	Time	%	pН		nit .		· · · · · · · · · · · · · · · · · · ·	1			lb per			· · · · · · · · · · · · · · · · · · ·	
	min	Solids		us	ed	Z-6	C.A.	Na2C03	Nazsio.	Na ₂ S	NaCN	ZnS04	404	3037	CuSO ₂
Grind (53.7%-200 m)	15	67		7 x 3	<u>14 RM</u>										
Condition	5	50	6.7	1000	-g cell	0.10	0.04								
No. 1 Pb float	3	30	6.5												
Condition	5		7.5		<u></u>			3.0	1.0.	1.0	0.20	1.00			
No. 2 Pb float	_14		8.0	1		0.10							0.20		
Zinc condition(1).	5		9.8			0.10		6.0	8.0				0.20		1.0
Zinc float Zinc clean	5			. 						18.0				0.80	
	Tw	<u> </u>		<u> </u>		I YSIS	0/ 24	<u> </u>		11		CTDI	JUTION		<u> </u>
PRODUCT	%	31		Pb	ZN	1515	<u>70 ^</u>					Pb	ZN	~~~	
No. 1 Pb conc No. 2 Pb conc Combined Pb conc (calcd Cl Zn conc Cl Zn tail Rougher Zn conc (calcd) Rougher tail Feed (calcd)) 17. 22. 46. 23.	.6 .5 .0 .4	28 34 13 20 2	4.95 1 3.51 2 3.63 1 0.19 2 2.38	8.27 16.48 14.66 21.65 .8.54 20.61 9.13 .8.41						2 3 4 1 6	5.6 9.2 4.4	2.2 15.7 17.9 54.7 23.7 78.4 3.7 00.0		
REMARKS: * From Inter (1) Addit						l	1b./t	0n	<u> </u>		l		<u>.</u>	1	

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TEST NO. 53 S	AMPL	MPLE: Cadillac Exploration Sample No. 2, Lots 32, 33 and 34 DATE: May 12, 1970														70		
OBJECT OF TEST: Zinc Recovery											CHARGE: 1000-g							
													TESTED BY: W.A.W.					
		ime	%	Ha		Unit	Reagents, Ib per ton											
		min [.]	Solids	pi		used		A.31	C.A.	Na2CO2	Na2SD3	NaCN	ZnSO	4 404	Na ₂ S	3037		
Grind (53.7%-200 m)		15	67		7 2	14 RM												
										······································								
Condition		5	50	6.		0-g cell	0.10	0.06	0.015									
Pb flotation No. 1		5	30	6.8	3											<u> </u>		
· · · · · · · · · · · · · · · · · · ·												ļ	ļ					
Condition		5.	30	7.3	3					2.0	1.5	0.2	1.			 		
Pb flotation No. 2							0.20					·		0.40	<u>بار</u>			
(1)						<u></u>		·						0.2				
Condition(1)		5	25	10.	2						12.0			0.2	2			
Zn flotation No. 1		5		11.()			0.04	`			·			15.0	1.0		
Zn flotation No. 2		3		11.(······	· ·	0.04							12.0	0.5		
	1	W				ANAL	YSIS					STRIBUTION %						
PRODUCT		%			РЪ	Zn				1		P	b	Zn				
·					·			•										
No. 1 Pb conc		22. 14.	9 -		36.61 42.05	15.16							8.3	18.7 10.4				
No. 2 Pb conc		14.	5		42.0J	13.30		ł						10.4				
Combined Pb conc (c	alcd)	alcd) 37.4			38.72	14.46		·. ·				6	6.2	29.1				
No. 1 Zn conc		25.4			25.10	20.85						2	9.1	28.6				
No. 2 Zn conc		4.7			8.52	20.55	ľ						1.8	5.2				
					- · · ·													
Combined Zn conc (calcd)		30.1			22.51	20.80	•.					3	0.9	33 .8				
Rougher tail		32.5			1.92	21.14							2.9	37.1				
Feed (calcd)		100.0			21.88	18.54						10	0.0	100.0				
• •								-					l					
					·													
REMARKS: * From I		1 Pc	II Dort M	S - 10	2-70-56	<u> </u>	1		ļ	<u> </u>			1		<u>L.,</u>			
(1) Additional R	leagent	s; N	aOH -	5.0,	Ammo	Phos, -	4.0; C	uS04 -	2.0 11	/ton.								