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Report No. 248

Concentration of lead-zine tailings from the dump at the Notre Dame (Tetreault) mine, Notre Dame des Anges, Quebec

C. 3. Parsons

Shipment: & shipment consisting of a carload of tailings was received at the laboratories February 8th. 1926 from the British Metal Corporation (Canada) Ltd. Montreal, Que. The material was taken from the tailing dump at the Botre Dame (Tetreault) mine at Notre Dame des Anges, Que.

Character of The dump consists of table tailings produced during material:

the operation of the mine by Meesrs. Tetreault Bros.

and when under lease to the Zinc Co. Ltd. The tailings are comparatively coarse and contain very little slime. They have not been affected to any extent by oxidation.

Purpose of The sample of the dump was submitted with a request that tests:

flotation tests be made to determine whether the zinc and lead, together with the small amount of silver and gold present could be economically recovered by this method of treatment. A flotation plant treating the run of mine ore is at present in operation at the mine and it is proposed that the old tailings could be treated in the same plant, either mixed with the ore or treated in a separate unit which is already available.

Test No. 1: This is a large scale tonnage test. The tailins were fed to a 42-ft. Hardinge mill charged with 1800 pounds of steel balls. A selective separation of the lead and zine was attempted. The pulp from the mill was delivered to an 8-cell Greenawalt mechanical agitation flotation machine. A lead concentrate was taken from one cell and the concentrate from the remaining cells was returned as a



middling to the feed end of the machine. The tailing from the lead cells was pumped to a Callow flat bottom unit consisting of two roughers operated in parallel and two cleaners in series. The tailing from each cleaner was combined and returned to the roughers.

Results: Amount of material run 4,440 lbs. Total time of running 4 hours Average feed per hour 1,110 lbs. Total lead conc. produced 116 1bs. Total zinc cone. produced 500 lbs. Lead 0.67% Zino 9.96% Lead 15.34% Zino 11.72 % Copper 3.92% Silver 31.7 Heads Lead conc. (sample whole run) Silver 31.7 oz Gold 0.20 oz/ton Zinc conc. (sample whole run) Sinc 43.16% Lead 0.35% (sample 1 to 3 pm) (sample whole run) 47.13 0.35 Tailing 0.35% Acid coal tar crecsote 0.35 "
Sod. cyanide 0.20 "
Cresylic acid Reagents: Lead flotation Cresylic acid 0.15 11 Copper sulphate 1.5 Zino flotation 0.3 Xanthate -Pine oil 11

Test No. 2: The same flow sheet was used as in test no. 1, but particular attention was given to the operation of the lead cells in order to raise the grade of the lead concentrate.

6,600 lbs. Results: Amount of material run 5.58 hours 1,182 lbs. Total time of running Average feed per hour 149 lbs. 1,031 lbs. Total lead cono. produced Total zinc conce produced Heads Lead 0.7% Zinc 10.06% Lead 0.7% Zinc 10.00% Lead 15.34% Zinc 10.20% Copper 3.92% Lead 22.81% Zinc 10.41% Copper 4.23% Zinc 49.09% Lead 0.14% 0.40% 0.06% 47.38% 0.44% 0.48% 0.10% Lead conc. (sample 10.50 -11.40am) Lead conc. (sample 11.40-3.20pm) Zino conc. (sample 10.50-11.40am) Tailing Zino conc. (sample 11.40-3.30 pm) Tailing 2.0 lb/ton Lead flotation Reagents: Soda ash 0.35 Acid coal tar creosote # Sodium oyanide 0.09 0.6 Caustic soda

Acid coal tar crossote 0.35 "
Sodium cyanide 0.09 "
Caustic soda 0.6 "
Cresylic acid 0.6 "
Copper sulphate 1.5 " Zinc flotation
Xanthate 0.20 "
Pine oil 0.15 "

Test No. 3: In this test the lead was floated in the Callow unit and the zinc in the Greenawalt machine. The object of the change was to try and raise the grade of the lead concentrate by the double cleaning action available in the Callow unit. It was necessary to use the Dorr classifier in closed circuit with the Hazdinge mill in order to obtain

Results: Amount of material run

in order to obtain an even distribution of the feed to the two Callow cells. In such a short test considerable fine lead is trapped and held in the classifier circuit and there is not sufficient time for the circuit to build up, hence the weight of the lead concentrate will be less than in the preceeding tests.

6640 lbs.

	Total time of running Average feed per hour Weight of least concentrate Weight of zinc concentrate		5½ hours 1,208 lbs. 137 lbs. 744 lbs.				
	Heads assay Lead conc. (sample Lead conc. Zinc conc. " Tailing " Zinc conc. " Tailing "	11am-2pm) 2pm-3.30pm 11am-2pm " 2pm-3.30pm	L	9000	771 037 76 05 05 09		10.15% 7.67% 7.09 49.62 0.88 46.83% 0.14
Reagents:	Acid coal tar creosote Sodium cyanide Cresylic acid Copper sulphate		2.8 1bs 0.45 0.10 0.15 1.5 0.25	ton H H H		flota	

Summary & Conclusions: The zinc can readily be recovered from the dump tailings by flotation. There was some difficulty at times in maintaining a froth which could be brought over the sides of the cells, but as a rule this condition could be adjusted by increasing the quantity of pine oil.

It is possible to obtain a lead concentrate containing over 30 ozs. silver and 3 to 4 per cent copper, but low in lead - the best grade made was 22.8% A quantity of gangue floated with the lead and prevented a higher grade concentrate being obtained. It is possible that on a larger tonnage basis the concentrate can be held back in the cleaner cells and a better cleaning action obtained, thereby producing a higher grade concentrate.